



DETERMINATION OF THE MAINTENANCE REQUIREMENTS OF ACTIVATED SLUDGE

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ABSTRACT

Maintenance energy plays an important role both in basic kinetic studies and in process development. Numerous studies have been devoted to the maintenance concept in various microbial fields but very few in biological wastewater treatment. Using a fermenter coupled to a mass spectrometer, we investigated the influence of the ratio S_0/X_0 (ratio between initial substrate concentration and initial biomass concentration) on the observed sludge growth yield of an oxic-settling anaerobic (OSA) system. By measuring the substrate removed, the oxygen consumed and the carbon dioxide produced, we were able to estimate the substrate fraction used for maintenance purposes. The results indicate that at a high S_0/X_0 ratio, a greater proportion of the substrate is devoted to maintenance thus significantly decreasing the observed growth yield. These findings are of particular importance in view of the cost associated with the disposal of excess sludge in aerobic wastewater treatment processes.

KEYWORDS

Activated sludge; maintenance requirements; growth yield; mass spectrometer.

INTRODUCTION

Organic substrate requirements have frequently been divided into requirements for growth and maintenance (Pirt, 1965). From a substrate balance, Pirt deduced a relationship between the apparent yield coefficient Y and the growth rate μ in continuous cultures :

$$1/Y = m/\mu + 1/Y_x \quad (1)$$

or

$$rs/X = \mu/Y_x = m \quad (2)$$

where Y_x is the theoretical (maximal) value of the growth yield coefficient, m the maintenance coefficient and rs the consumption rate of the substrate. These equations have only been used in the continuous system.

Numerous studies have been devoted to the maintenance concept in various microbial fields but very few in biological wastewater treatment. The aim of this study is to apply the maintenance concept to studies of activated sludge growth for estimating their maintenance requirements.

MATERIALS AND METHODS

A respirometric system consisting of a quadrupole mass spectrometer (QMS) coupled to a 15 l fermenter[®] (Chang, 1988; Chudoba *et al.* 1991) has been used throughout this study. All our experiments were run aerobically and the inoculated activated sludge came from a continuous oxic-settling-anaerobic system (OSA). The experimental program was based on different ratios of the initial substrate concentration (S_0) to the initial biomass concentration (X_0). By means of this respirometric system, oxygen uptake, carbon dioxide production, activated sludge growth and substrate removal have been measured simultaneously.

RESULTS AND DISCUSSIONS

The substrate balance has been done by:

$$\Delta S = \Delta S_m + \Delta S_x \quad (3)$$

where ΔS is the total quantity of substrate utilization, ΔS_m is the quantity of substrate utilization for maintenance and ΔS_x is the quantity of substrate utilization for growth. Dividing this equation by the total quantity of biomass produced (ΔX), we obtain:

$$1/Y_{obs} = 1/Y_x + f_s * \Delta S / \Delta X \quad (4)$$

where Y_x is the theoretical (maximal) growth yield coefficient, and f_s is the $\Delta S_m / \Delta S$ ratio. By rearranging this last equation, we obtain the following equation:

$$1/Y_{obs} = 1/Y_x - f_s * (S_{min}/X_0)/(X_{max}/X_0 - 1) + f_s/(X_{max}/X_0 - 1) * (S_0/X_0) \quad (5)$$

where S_{min} is the residual substrate concentration and X_{max} the final (maximal) biomass concentration. From our experimental results (Fig. 1), we have obtained a linear relationship as:

$$1/Y_{obs} = a * S_0/X_0 + b \quad (6)$$

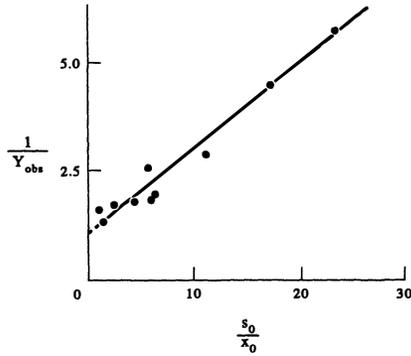
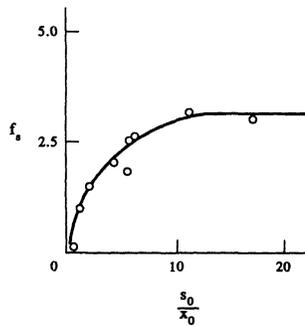
Comparing the equations (5) and (6), we obtained the following relations:

$$a = f_s (X_{max}/X_0 - 1)$$

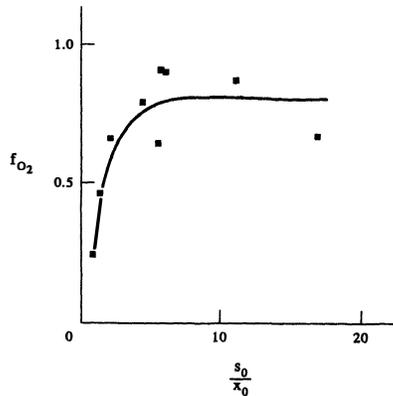
and

$$b = 1/Y_x - f_s * (S_{min}/X_0)/(X_{max}/X_0 - 1)$$

By applying equation (5), we calculated f_s and Y_x . The values of f_s varied with the ratios of S_0/X_0 (Fig. 2) and the values of Y_x were constant. This theoretical value was $Y_x = 0.88 \pm 0.095$ mg SS/mg TOD, or 2.7 ± 0.22 mg SS/mg TOC.

Fig. 1. Influence of S_0/X_0 on $1/Y_{obs}$.Fig. 2. Influence of S_0/X_0 on f_s .

Using the same method, similar curves were also obtained for O_2 (f_{O_2}) and CO_2 (f_{CO_2}) (see Fig. 3 and 4). It means that the higher the S_0/X_0 ratio, the greater is the proportion of the substrate used for maintenance purposes and the smaller is the observed growth yield. In our experiments we found that at a very high S_0/X_0 ratio, 64% of substrate removed was used for maintenance requirements. This phenomenon was also observed by Pirt (1975) and Moletta (1979). Chudoba (1991) also found also in the continuous OSA system, the specific sludge production rate (g SS/g DCO) decreased with a mass loading increase.

Fig. 3. Influence of S_0/X_0 on f_{O_2} .

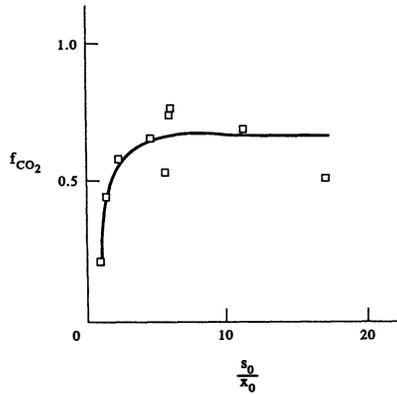


Fig. 4. Influence of S_0/X_0 on f_{CO_2} .

CONCLUSIONS

The results obtained in this study show that under batch conditions the observed biomass yield (Y_{obs}) decreased with an increase in the S_0/X_0 ratio for activated sludge samples originating from an OSA system. By applying the maintenance concept in our studies, we calculated the substrate utilization, oxygen uptake and carbon dioxide production for maintenance energy requirements. The proportion between anabolism and catabolism of the activated sludge depends on the S_0/X_0 ratio. These observations give us another idea for reducing the excess activated sludge production since in wastewater treatment, a considerable part of the total cost is used for the treatment of excess sludge. If a treatment system can be in favour of the maintenance of activated sludge, the excess activated sludge will be much reduced.

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