

An assessment of the use of native and denatured forms of okra seed proteins as coagulants in drinking water treatment

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ABSTRACT

The effects of temperature, storage time and water pH on the coagulation performance of okra seed protein in water treatment were assessed. In a jar test experiment, okra salt extract achieved a notable improvement in treatment efficiency with storage time and showed good performance in quality after thermal treatment at 60, 97 and 140 °C temperatures for 6, 4 and 2 hours, respectively. The performance improvement of more than 8% is considered to be due to the denaturation and subsequent removal of coagulation-hindering proteins in okra seed. Furthermore, the results of a sodium dodecyl sulphate polyacrylamide gel electrophoresis analysis show two distinctive bands of protein responsible for the coagulation process after denaturation. It was further shown that at optimal coagulant dose, the pH of the treated water remained unaffected as a result of the protein's buffering capability during coagulation. Therefore, denatured okra seed exhibited improved performance compared to the native crude extract and offers clear benefits as a water treatment coagulant.

Key words | coagulation, denaturation, okra, protein, seed, water treatment

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INTRODUCTION

Background

Water treatment improves the quality of water supplied to the general public by eliminating pathogens, turbidity and other contaminants in the raw water that may be harmful to human health. The availability of good drinking water at all times enhances human development and reduces the risk of contracting diseases that can emanate from polluted or contaminated water. However, many communities in developing countries lack adequate access to potable source of drinking water, with over 748 million people living in poverty still lacking access to clean water for domestic use (WHO & UNICEF 2014). In sub-Saharan Africa alone, the number of communities that are not supplied with safe water today remains higher than in the 1990s. Thus, water remains one of the greatest threats to mankind in the developing world. Water-related disease has claimed over 1.8 million lives annually, mostly those of children under five years of age

(WHO 2007). Efforts by government at all levels to tackle this problem have failed in many developing countries due to lack of funds. Providing good water infrastructure and skilled personnel to improve domestic water quality will save the lives of many people in rural areas. To achieve this, coagulation and flocculation as a means of domestic water purification should be enhanced. These processes are employed essentially to improve the aggregation and settlement of particles that are later removed from sedimentation and filtration units. The process is, however, dependent upon the ability of the coagulant and flocculant aids to produce flocs with suitable characteristics. Coagulant and flocculant mixing processes play a vital role in the transformation of particles into flocs (Duan & Gregory 2003) and the subsequent bridging of the flocs into bigger macro flocs. Aluminium sulphate and ferric chloride are globally the most widely used coagulants in drinking water treatment (Duan & Gregory 2003). However, the presence of residual

doi: 10.2166/wh.2016.015

aluminium (Al) in the final water has posed some concern to water and wastewater operators (Driscoll & Letterman 1988), as prolonged ingestion of aluminium in water has been linked to the development of cognitive decline in the human brain and Alzheimer's disease (Gauthier *et al.* 2000). Martyn *et al.* (1989) reported that the rate of Alzheimer's disease in England and Wales was higher in areas where the mean aluminium concentration exceeds 0.11 mg/l than in locations with less than 0.01 mg/l. Furthermore, some chemical polymers, e.g. acrylamide, are thought to be carcinogenic (Mallevalle *et al.* 1984). In addition, the application of aluminium sulphate in water treatment can consume the alkalinity and pH of the treated water that may result in reduced coagulation efficiency.

However, in many developing countries, indigenous materials of natural plant and animal origin have been used for decades in household water treatment. These materials, if properly applied, have significant potential to increase the efficiency, and reduce the overall cost, of water treatment. Natural plant seeds are biodegradable, widely available, environmentally friendly, and are non-toxic when consumed as food. Examples of natural plant species previously studied include *Moringa oleifera* (MO) (Jahn 1988; Ghebremichael *et al.* 2005), cactus (Zhang *et al.* 2006) and mustard seeds (Bodlund *et al.* 2014). Jahn (1988) used MO seed extract as a coagulant to alleviate domestic water supply problems in the developing world. Madsen *et al.* (1987) also used MO extract as coagulant and observed 99.5% reduction in turbidity accompanied by 80–99% reduction in coliform and faecal coliform count. Additionally, it has been reported that the coagulation potential of cactus plants is comparable to that of aluminium sulphate in removing turbidity in water with low dose (Zhang *et al.* 2006). Similarly, Bodlund *et al.* (2014) investigated the performance of different mustard seeds in pond and synthetic water and reported a coagulation activity of greater than 70% in mustard (large) compared to 60% in mustard (small), whereas mustard (yellow and cake) achieved 45 and 25%, respectively. To date, most research has focussed on the crude seed extract and the purified seeds' proteins. Although MO has received more attention by researchers than the other plant seeds, there are potentially many vegetable plants that could perform as effectively and efficiently as MO in raw water treatment.

Extent of okra plant applications

Okra is a plant widely grown in Nigeria and many other tropical regions of the world because of its nutrients and ease of cultivation. It can grow under different environmental conditions and reach maturity within three months of planting. Okra seed is a major source of protein, vitamin, calcium and oil, and is capable of curing ulcers and providing relief from haemorrhoids (Abidi *et al.* 2014). The okra pod contains carbohydrate and mucilaginous substances capable of removing turbidity in water, treating tannery and industrial wastewater (Agarwal *et al.* 2003). In their separate studies, De Jesus *et al.* (2013) and (Patale *et al.* 2012) applied okra powder obtained from a mature pod and achieved up to 99% reduction in turbidity within 10 minutes sedimentation time, due to the presence of mucilage substances in the pod. Conversely, the application of mallow and mucilage obtained from okra plants in water treatment revealed a major drawback due to the addition of organic substances from the plant in the final water (Anastasakis *et al.* 2009). Furthermore, the flocculating performance of various parts of okra plant, including the seed, was studied by Fahmi *et al.* (2014) on 55 NTU kaolin water and observed that only a 64.5% reduction in turbidity was achieved with okra seed extract. Okra is one of the most consumed traditional vegetables, eaten fried or boiled, steamed and may be added to salads, soups and stews. The extracted mucilage of the okra pod is used as a suspending agent and as a pharmaceutical adjuvant in paracetamol and other drug delivery (Sharma *et al.* 2013; Zaharuddin *et al.* 2014). It is also widely used in the cosmetic, pharmaceutical and food industries as a preservative.

In natural plant seed extracts, the coagulating compounds reported in the literature concern cationic protein (Ghebremichael *et al.* 2005). Studies have found the protein content in defatted okra seed to be as high as 40–50% (Oyelade *et al.* 2003), whilst in crude form, okra seed protein content was found to be in the range of 23.8%–25.5%. Protein, in a cationic state, can easily precipitate from solution with negatively charged substances. Okra seed protein contains over 100 amino acids and more than eleven major amino acids including three positively charged (arginine, lysine and histidine), and the two anions of aspartic and glutamic acids (Sami *et al.* 2013). The ϵ -amino group, the guanidine group and the imidazole

group of the corresponding lysine, arginine and histidine residues in okra can give proton alkaline characteristics; they can bind the hydrogen ion and provide the protein molecule with a positive charge after they are fully ionised.

Protein denaturation

A protein is said to become denatured when its folding structure is altered as a result of exposure to certain elements of physical factors (e.g. heat), causing the protein to become biologically inactive. Proteins also degrade and denature upon storage, with such denaturation leading to visible aggregation and turbidity formation (Sharma & Luthra-Guptasarma 2009). In some instances proteins can be rena-tured but in most cases the denaturation is irreversible.

The research reported in this paper evaluates the per-formance of denatured Okra seed protein compared to its native state as an alternative water treatment coagulant and disinfectant in domestic water purification.

MATERIALS AND METHODS

Collection and preparation of the okra seed

A good quality seed of okra was obtained at a local market in Hawul local government area of Borno State, Nigeria. In this market, fresh and old seeds of high quality species of okra are readily available. The seeds were sorted, packaged and labelled appropriately for ease of identification and transported to the UK for laboratory processing, preparation and analysis. The seed was cleaned by washing with tap water in order to remove contaminants such as dust, damaged seeds and plant debris which might affect the integrity of seeds during water treatment. The seeds were then dried in an oven at 60 °C for 6 hours before grinding.

Chemicals and reagents

Analytical grade chemicals and reagents (sodium chloride, sodium hydroxide, aluminium sulphate and hydrogen chlor-ide) were obtained from Fisher Scientific, UK and kaolinFluka-60609, from Sigma Aldrich, Germany. Deionised

(DI) water was used to prepare all the suspensions and con-centration solutions in this study.

Preparation and extraction of active compound in okra seed

The seeds of okra were ground to fine powder using a lab-oratory miller (Tema mill, Germany) for 2 minutes to obtain the desired powder. The resulting seed powders were sieved through a set of stainless steel sieves (600 to 212 µm). The powders retained on the 212 and 300 µm were combined and used in the study.

The extract was prepared from the ground seed powders by adding 1.0 M NaCl solution to the seed powder to make 2% (w/v) suspension, i.e. 2 g of the seed powder in 100 ml NaCl. The suspension was vigorously stirred using a magnetic stirrer for 15 minutes at room temperature (19 ± 2 °C). In many tropical countries, room temperature ranges between 22 and 25 °C. The suspension was then centri-fuged at 4,000 rpm for 10 minutes using a Heraeus Megafuge16 (Thermo Scientific, Germany). The suspension was decanted and the residual solids were dried in an oven at 50 °C overnight. The weight of the dried solid material was measured to ascertain the amount of seed powder used in making the suspension. The decanted suspension was then fil-tered through a Whatman No. 42 filter paper and the filtrate termed okra salt extract (OSEX). Similarly, the extract was pre-pared by dissolving 2 g of the seed powder in 100 ml of DI water to make 2% suspension, to extract the coagulating com-pound in the seed. The suspension was stirred using a magnetic stirrer for 15 minutes and then centrifuged at 4,000 rpm for 10 minutes. The suspension was decanted as in OSEX and then fil-tered through a Whatman No. 42 filter paper and the filtrate termed okra water extract (OWE). In addition, 2 g of MO was dissolved in 100 ml NaCl to make 2% suspension of MO extract and used in the study. Protein concentration in the extracts was estimated following Bradford (1976) with standard bovine serum albumin (BSA), absorbance was measured at 595 nm using Ultrospec 2100, UV/visible spectrophotometer.

Denaturation of OSEX

The OSEX solutions were heated using a hot plate at tempera-tures of 60, 97 and 140 °C for 6, 4 and 2 hours, respectively.

The wide temperature range was selected because most people in developing countries use firewood as a source of cooking energy which is difficult to control. The heated samples were then centrifuged at 4,500 rpm for 10 minutes and were filtered through a Whatman no. 42 filter paper and used in the study. Similarly, the extract was stored for 1, 3, 7, 10 and 14 days to denature the extract. Finally, the molecular weight (MW) of the extracts and the denatured protein samples were determined on 12% sodium dodecyl sulphate polyacrylamide gel electrophoresis (SDS-PAGE).

The protein sample was resolved by SDS-PAGE (normal PAGE) and transferred to a nitrocellulose membrane (Protran BA-85, Pierce Protein Biology). The membrane was blocked in 5% milk/1X TBST (Tris-buffered Saline-TWEEN 20) and incubated on a rocker at room temperature for 30 minutes. After the blocking, the membranes were incubated with primary antibody polyclonal goat anti-GFP (AbD Serotec) 1:2000 of antibody in TBST overnight at 4 °C. At the end of the incubation, the membranes were washed three times with TBST at 5 minutes interval each and then incubated with the secondary antibody (polyclonal anti-Goat HRP) 1:1000 of antibody in TBST for 1 hour at room temperature on a rocker. The membranes were washed again as performed at the end of primary antibody incubation. The blots were then incubated with West Pico Chemiluminescent Substrate (Pierce) and then visualised with Gene Snap Software (SynGene).

Water samples for coliform and *Escherichia coli* tests

Natural water samples were collected from the Bourn Brook River adjacent to the University of Birmingham in order to determine the bacterial inactivation capability of the heated OSEX on coliform count and *E. coli* present in the water. The river water was spiked with kaolin to bring the turbidity level to 45 NTU. After the jar test, the experiment was conducted using Colilert-18/Quanti-Tray (IDEX Inc., UK) for coliform/*E. coli* detection because of its ease of operation, flexibility, accuracy and speed. Colilert 18 was added to the water sample in a 100 ml sterilised vessel and the mixed reagent was then decanted into a tray, sealed and incubated at 35 °C for 18 hours. The presence of *E. coli* was determined with the help of a UV probe. The number of positive wells was counted and then read off on the most probable number

(MPN) chart provided by IDEXX. The water sample was treated with two ranges of OSEX doses (50 and 80 mg/l) and the results compared with aluminium sulphate as a coagulant. The performance of OSEX in a natural water environment in terms of turbidity removal was also evaluated.

Preparation of the synthetic turbid water

Turbid water samples for jar test experiments were prepared by adding kaolin particles into tap water. 40 g of laboratory grade kaolin (Fluka, and high grade, Sigma-Aldrich) was added to 400 ml of tap water and the suspension stirred for 30 minutes using a magnetic stirrer. The suspension was made up to 1 l by adding 600 ml of tap water and then stirred for further 30 minutes. The suspension was allowed to stand for 24 hours for the kaolin to hydrate. The suspension was vigorously mixed for 5 minutes and the contents mixed with 30 l of tap water and allowed to stand overnight for particle settlement. The supernatant was decanted and its turbidity measured. Depending on the level of turbidity required, the supernatant was either diluted with tap water or concentrated with kaolin suspension. Turbidity and pH were determined as initial values using standard methods before conducting the jar test experiments. Buffer capacity (BC) was calculated according to [Morr *et al.* \(1973\)](#),

$$BC = \frac{\text{titrant (mg)}}{\text{wt of protein}} \times \Delta pH \quad (1)$$

Coagulation and flocculation test

Jar tests were conducted using standard apparatus comprising six 1 litre beakers (Phipps & Bird, 7790-900B USA) to evaluate the optimum coagulant dose for the coagulation tests. For effective dispersion of the coagulant, the water was rapidly mixed at 200 rpm ($G = 240 \text{ s}^{-1}$) for 1 minute during which various doses of the coagulant were added to the beakers. The mixing speed was then reduced to 30 rpm ($G = 23 \text{ s}^{-1}$) for a further 30 minutes to simulate the flocculation stage. The suspension was then allowed to stand undisturbed to facilitate settlement for 1 hour. A final treated water sample (10 ml) was drawn 2 cm from the top surface of the water in the beakers using a syringe. The turbidity of the water was then measured using a turbidity meter (HI 93703, Hanna)

and the water pH was measured with a pH meter (Mettler Toledo SevenGO, Switzerland). All experiments were conducted at room temperature ($19 \pm 2^\circ\text{C}$).

RESULTS

Coagulation performance of native (non-denatured) okra extracts

The effect of varying native OSEX dose on turbidity removal was investigated, and results are shown in Figure 1. Different doses (0–80 mg/l) were applied to synthetic turbid water with two levels of turbidity, 100 and 200 NTU using a standard jar test procedure. The advantage of using the synthetic turbid water over river water was that it enables the study to simulate the different levels of turbidity in water. The lowest residual turbidities were achieved with 40 mg/l (100 NTU) and 60 mg/l (200 NTU) doses of OSEX, with corresponding removal efficiencies of 91 and 98%, respectively. Furthermore, it was observed that at coagulant dose higher than 40 mg/l, there was no reduction in residual turbidity in water with 100 NTU. Similarly, when the coagulant dose in the high turbidity water (200 NTU) exceeded 60 mg/l, residual turbidity exhibited a modest increase. In addition, the study investigates the removal of turbidity in water with 100 and 200 NTU using OWE as shown in Figure 2. The result shows that DI water extract did not yield any significant performance at the end of the treatment process. Minimum residual turbidity was 67.25 NTU, representing only 33% turbidity removal efficiency, using 40 mg/l dose of OWE sample while in the 200 NTU water, final residual turbidity was 160 NTU, representing

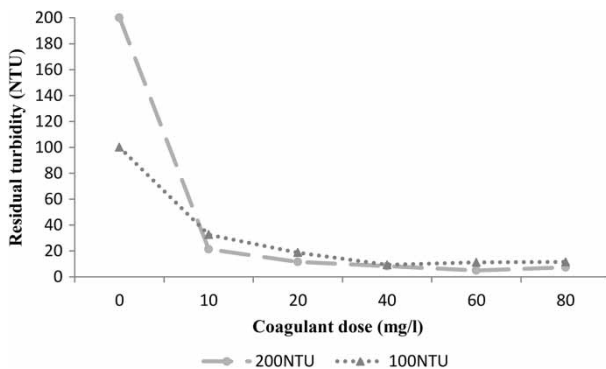


Figure 1 | Performance of OSEX as a coagulant in treating turbid water.

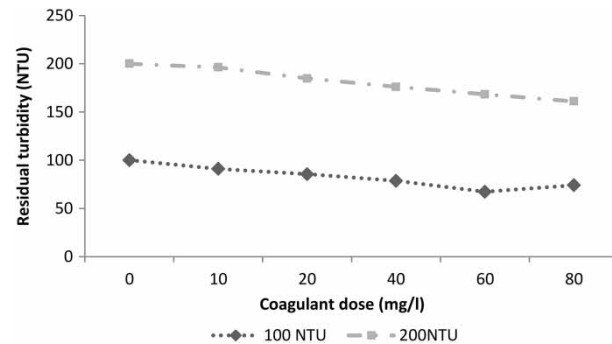


Figure 2 | Performance of OWE as a coagulant in treating turbid water.

approximately 20% efficiency at maximum dose of 80 mg/l used in the study. Further coagulant addition in the 100 NTU water also resulted in re-stabilisation of colloids in water, indicating poor performance beyond 40 mg/l. The typical protein concentration in OSEX was 1.018 mg/ml and 0.264 mg/ml in OWE. Therefore, the poor performance in OWE show that DI water is not a strong solvent, aggressive enough to extract okra seed proteins while NaCl solution was observed to be very effective in this regard due to salting.

Effect of pH change on the performance of the OSEX

Different pH values were assessed in order to determine the optimum coagulation and flocculation pH because of its importance in water treatment and also as it affects the stability of the protein. The OSEX dosage that achieved maximum turbidity removal was then investigated. In addition, the effects of pH on the optimal dosage of the coagulant found in the earlier experiments were investigated. Specifically, different OSEX doses (40, 60 and 80 mg/l in the pH range 4–9) were assessed for turbidity removal on kaolin water with original turbidity of 200 NTU and the results are shown in Figure 3. Minimum residual turbidity was found at pH 4 and the maximum residual turbidity was found at pH 9 for the three doses. At pH 4, turbidity removals were 99, 98 and 97% for 40, 60 and 80 mg/l doses, respectively. The effect of coagulant addition on final water pH during the jar tests was considered for aluminium sulphate, MO and OSEX by incrementally dosing 10–100 mg/l of each coagulant to water with initial turbidity of 200 NTU. As the doses of each of the coagulants increased, the corresponding change in water pH was measured. Figure 4

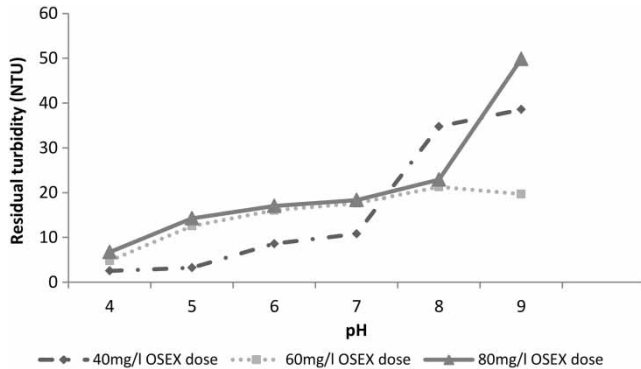


Figure 3 | Influence of pH on turbidity removal using an OSEX.

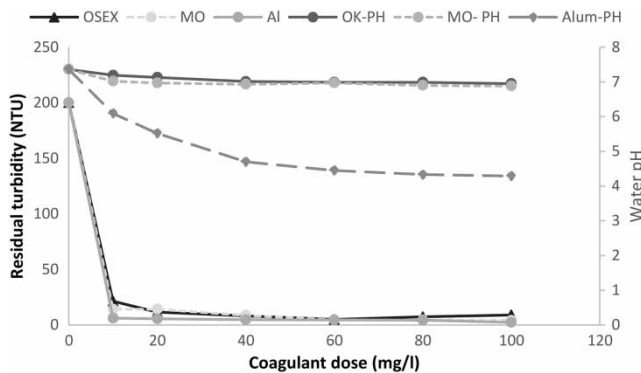


Figure 4 | Effect of different coagulants doses on final water pH and turbidity.

shows that the treated water pH was largely unaffected when the natural coagulants, MO and OSEX, were used. This is because the pH of the water was buffered due to the presence of protein in the seed during coagulation. The amount of protein used for coagulation was 6.11 mg in OSEX and 7.9 mg in MO with a BC of 0.016 and 0.017, respectively. However, alum dosing to 40 mg/l produced an approximately linear reduction in pH from an initial value of pH 7.5 to pH 5, followed by a reduced rate of pH change (pH 5 to pH 4.5 when dosed from 40 to 100 mg/l). Similarly, as the doses of each of the coagulant increases, the removal of turbidity also increases in MO and alum treated water until maximum dosage 100 mg/l was reached. The lowest residual turbidities in the final water of 4.29 and 4.08 NTU were achieved with alum and MO, respectively, and 4.89 NTU with an OSEX dose of 60 mg/l. The results show that all the coagulants achieved approximately 98% turbidity removal. Figure 4 shows that all the coagulants exhibited the same trend of behaviour in terms of turbidity removal. However, seed proteins are amphoteric and contain both the basic and

acidic amino groups which can buffer in solution. Thus, in water treatment processes, the relationship between the initial and the final water pH play an important role in determining the optimum pH required for coagulation.

Effects of denaturation by storage and temperature on the integrity of the OSEX

The effect of storage time on the performance of OSEX was considered in order to identify the most appropriate time stock solution of OSEX will take before any deterioration in quality as a coagulant. This is vital in developing countries, where electricity supply is a major challenge, and the cost of obtaining modern, temperature-controlled storage facilities is prohibitive. Fresh OSEX was prepared and then stored in 200 ml open beaker at room temperature of $19 \pm 2^\circ\text{C}$ between 1 and 14 days intervals to observe its denaturation process. Performance was assessed using OSEX which had been stored for 1, 3, 7, 10 and 14 days. Figure 5 shows that the performance of OSEX as a coagulant increased with storage time to day 10, after which its effectiveness, in respect of turbidity removal, deteriorated. Optimum performance was observed when OSEX was dosed at 40 mg/l. This yielded a reduction of 92% from 130 NTU to less than 10 NTU. The coagulation performance at 60 mg/l dose was the same as that of 40 mg/l, and deterioration was observed when dose exceeded 100 mg/l.

The effects of temperature variation to denature the OSEX sample and its performance when treating synthetic water of initial turbidity of 200 NTU were considered by heating the extract to 60°C for 6 hours, 97°C for 4 hours and 140°C for

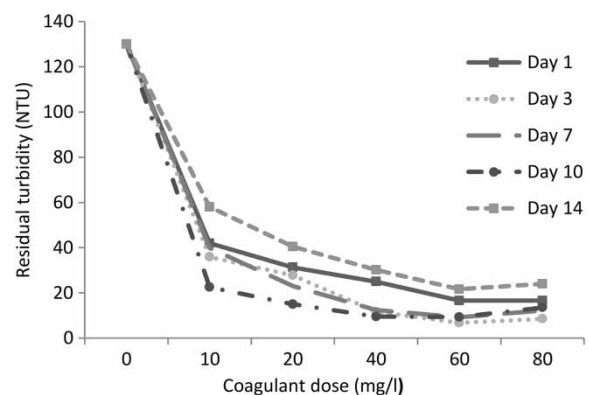


Figure 5 | Removal of turbidity in synthetic water using stored OSEX.

2 hours (Figure 6). Under this condition, all the extract samples were used immediately after preparation (fresh). The results show that at 80 mg/l, maximum turbidity removal efficiencies of >97% were recorded with all the denatured extracts, whereas a maximum efficiency of 93% was recorded with non-denatured extract. However, at lower coagulant dose, 10 mg/l, turbidity removal efficiency of the unheated extract was approximately 80% while the heat-treated samples recorded between 66% and 74% performance. It is noteworthy that when the performance of the heat-treated sample at 60 °C for 6 hours was applied at a higher dose of 200 mg/l to a very high turbidity water (550 NTU), the residual turbidity was observed to be 2.7 NTU representing a percentage removal efficiency of >99% (Figure 7). This is a typical water turbidity level in streams and rivers in the tropics, especially in sub-Saharan Africa after a rainfall event. Therefore, it is important to investigate the performance of OSEX on very high turbidity water for people in developing countries.

SDS-PAGE analysis of the three samples

SDS-PAGE analysis was conducted on the OSEX in order to obtain information on the extract and the denatured samples as well as to determine the MW of the different fractions of OSEX. Here, OSEX denatured by heating and OSEX denatured by storage together with non-denatured OSEX were analysed in order to provide information regarding the stability of the different protein sizes after exposure to high temperature and storage. The various bands and sizes of the proteins are depicted in Figure 8. The SDS PAGE results showed some similar distinctive protein bands with MW from 4 to 12 kDa in all the samples. Faint

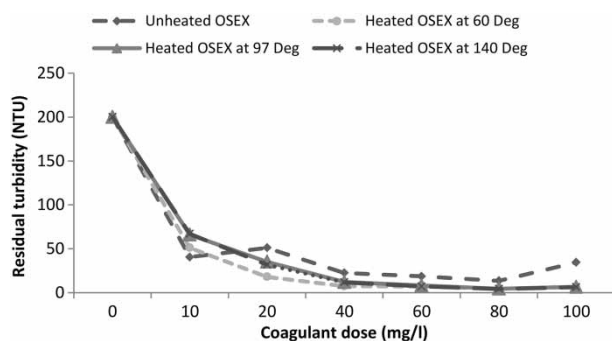


Figure 6 | Removal of turbidity in synthetic water using thermally treated OSEX.

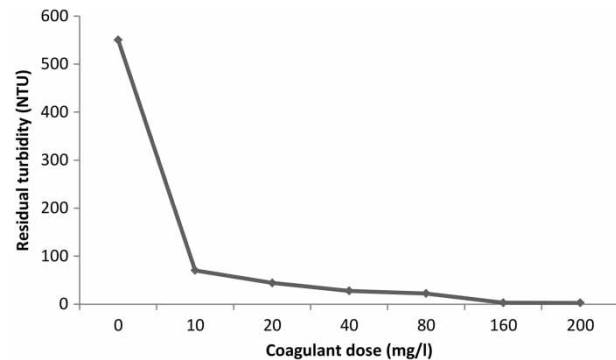


Figure 7 | Removal of turbidity in very high turbidity water using thermally treated OSEX.

bands were observed across the stored sample compared to the crude and heated extracts. However, the densest bands were found in the heated samples at MW of 20 and 45 kDa. Interestingly however, the band with MW 43 kDa of protein in the heated samples was not visible in either the crude extract or the stored samples. This is thought to be a result of the removal of some overlapping proteins during heating which were absent in both the crude and the stored samples. The concentration of proteins across all the bands is higher in the heated sample than in crude extract and stored samples. However, despite the faint band in the stored sample, the coagulation performance of the stored sample was found to outperform that of non-denatured sample.

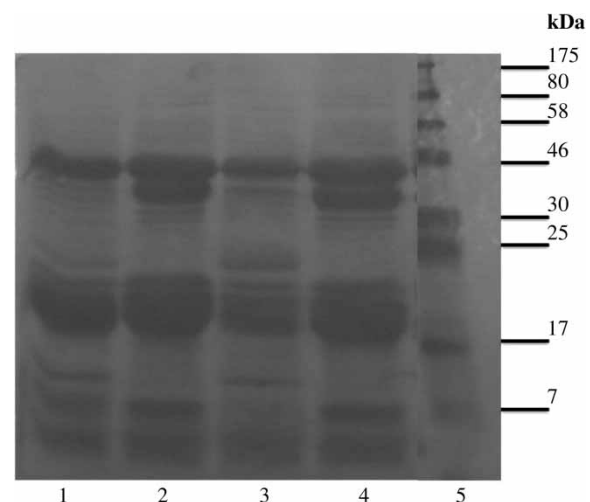


Figure 8 | Protein profiles of OSEX using 12% SDS-PAGE analysis. Lane 1 untreated OSEX; Lane 2 heat treated OSEX at 140 °C for 2 hours; Lane 3 stored OSEX sample for 3 days; Lane 4 heated OSEX at 60 °C for 6 hours; and Lane 5 a Marker (New England, BioLab).

Bacterial inactivation by okra crude extract

The results of the bacterial reduction of coliforms and *E. coli* count using OSEX are presented in Table 1. In this study, colilert-18 Quanti-Tray method was adopted to assess the bacterial quality of the raw water before and after treatment with OSEX, and the result compared with that of aluminium sulphate. It is noteworthy that the number of large and small positive wells for coliform were the same in the raw water, before and after treatment because of the multiple presence of microbes other than *E. coli*. In this case, the number of coliform counts was found to be 2419.6 MPN/100 ml in both raw and treated water. However, there was a substantial reduction in total *E. coli* count as observed in Table 1, using 50 and 80 mg/l coagulant dosages. *E. coli* is a subset of total coliform, hence, the result show that *E. coli* count/100 ml in the raw water before treatment was 727.0/100 ml while after treatment, the total *E. coli* count was reduced to 79.9/100 ml and 54.5/100 ml, giving a percentage reduction in *E. coli* count of 89% and 93%, respectively. In addition, at optimum coagulant doses of 50 and 80 mg/l, turbidity removals were 88% and 75%, respectively, in the final water. In both cases, there was no observed decline in total coliform count after

treatment, suggesting that some organic compounds in the seed were utilised as substrate by other microbes in the water to aid growth. Further investigation using aluminium sulphate as a coagulant achieved 86% reduction in *E. coli* count (from 727.0/100 ml to 102.2/100 ml) with a corresponding reduction of 28% in total coliform (from 2419.6 MPN/100 ml to 1553.1 MPN/100 ml). Similarly, there was substantial reduction in turbidity (approximately 98%) in final water treated with aluminium sulphate. The high removal of turbidity in alum treated water may be responsible for the reduction in total coliform count in this regard.

DISCUSSION

In the work reported here, OSEX in its native form was used as a coagulant in treating water with turbidity of 100 and 200 NTU. It was observed that an increase in OSEX dose resulted in a reduction of residual turbidity to a minimum value beyond which further addition of coagulant caused an increased turbidity as a result of re-stabilisation of the colloids (Figure 1). At this point, there were more positively charged species than the available surface charges on the colloids which encouraged stabilisation. At coagulant dose of 40–60 mg/l, maximum turbidity reductions of 91–98% were observed, as shown in Figure 1. Maximum removal efficiency was recorded in the high turbidity water (200 NTU) producing a residual turbidity of 4.9 NTU, a value which is compliant with the WHO and Nigerian drinking water standards of 5 NTU (SON 2007). This result is in agreement with finding reported by Katayon *et al.* (2004) who used MO extract to evaluate the performance of MO in low and high turbidity water. Turbidity removal was effective in high turbidity water because destabilisation is influenced by a high rate of colloidal interaction which encourages particle bridging (Gregory & Duan 2001).

In the work reported here, it was observed that OWE indicated poor performance in terms of turbidity removal. This means that DI water is not aggressive enough to extract the coagulating compounds while solvents such as NaCl solution were seen to be more aggressive in extracting the coagulating protein. Figure 2 shows that turbidity removal was 33% and 20% when OWE was used to treat 100 and 200 NTU water, respectively, compared with 91% and

Table 1 | Removal of coliform and *E. coli* count in river water using OSEX and AS

Parameters	Raw water	OSEX-50 mg/l	80 mg/l	Alum-treated
Initial water turbidity (NTU)	45	–	–	–
Treated water turbidity (NTU)	–	5.6	11.4	0.92
<i>Number of positive wells for coliform</i>				
Large wells	49	49	49	49
Small wells	48	48	48	45
Total coliform count (MPN/100 ml)	2,419.6	2,419.6	2,419.6	1,732.9
Percentage reduction in coliform count (%)	0	0	0	28
<i>Number of positive wells for E. coli</i>				
Large wells	49	31	29	44
Small wells	33	19	8	3
<i>E. coli</i> count (MPN/100 ml)	727	79.9	54.5	102.2
Percentage reduction in <i>E. coli</i> count (%)	89	93	86	

98%, respectively, achieved with OSEX. Furthermore, the protein concentration in OSEX was 3.8 times higher than that in OWE. The effectiveness of OSEX may be due to the salting-in effect in the salt extracts causing an increase in protein solubility and dissociation as reported by Okuda *et al.* (1999), because the NaCl solution has a substantial effect on the solubility of a protein.

To investigate further the character of okra protein, the relationship between coagulant doses at different pH as it affects protein stability was investigated, as shown in Figure 3, using the optimal coagulant doses obtained in the previous tests. The results showed the effect of turbidity removal at lower pH to be significant ($p < 0.05$), with a maximum of 99% efficiency removal at pH 4. This shows that low water pH had an important effect on the coagulation of turbid water with OSEX. Whilst it is not practical to treat water at such a low pH, OSEX has shown to perform effectively at pH of 6.5–7.5 as well. These were the ranges of water pH tested in the previous experiments. Each protein has an optimal pH to attain its biological function and its activity is normally affected by only a slight change in pH. Generally, an acidic environment is considered to be conducive to the binding of a proton from the dissociated carboxyl group and the transformation of protein into a cationic state, which is responsible for the charge neutralisation on particles in the water. It is known that inorganic particles are negatively charged in aquatic environments and the net surface charge of colloidal particles is reduced at low pH (Gregory 2005) which encourages the double layer compression. While study has reported that natural coagulants are most effective in coagulating water at pH in the region of pH 8 and above (Okuda *et al.* 2001), the study reported here observed the most effective pH to be lower, around pH 4. This demonstrates that the amino acid composition of proteins in different plants may have different coagulation activities. The difference in coagulating property may be attributed to the type of protein in okra seed although this requires further investigation.

The effect of coagulant addition on treated water pH and turbidity removal was investigated as shown in Figure 4. MO, the most studied natural plant; aluminium sulphate, a widely used synthetic coagulant in water treatment; and OSEX were each tested in water with a turbidity of 200 NTU. The results show that all the coagulants achieved approximately 98% turbidity removal efficiency with somewhat similar coagulation

action. Turbidity reduction increases as coagulant dose increases, indicating the level of charge neutralisation to be similar, though the performance of OSEX was not as effective as that of MO and alum due to its high lipid content. Furthermore, the results show that incremental dosing of both OSEX and MO extracts yielded a plateau curve nature, meaning that the pH of the final water remained unaffected from its initial pH of 7.36 whereas alum was found to depress the pH of the water to pH 4.3. In aqueous solutions, amino acids contain weak α -amino groups (basic) and weak α -carboxylic groups (acidic). Furthermore each of the basic and acidic amino groups contain in its side chain an ionisable group and so the combined actions of free amino acids and other amino acids in peptide linkages act as effective buffers during coagulation which resist a change in the pH of the water. Thus, natural coagulants offer an advantage over synthetic coagulants since no chemical addition is needed to control the pH of the treated water.

The efficacy and integrity of OSEX after denaturation was assessed based on different storage duration as shown in Figure 5, and temperature as indicated in Figure 6. Interestingly, it was observed that the coagulation efficiency of OSEX improved by approximately 8% with storage time from the third to tenth days, even though the increase was not appreciable and then degraded in quality thereafter. This suggests that, since there are many different sizes or bands arising from heterogeneity of one or more active proteins in seed (Ghebremichael *et al.* 2005), some of the proteins which were eliminated during the storage due to denaturation are protein compounds that hinder coagulation activity. However, the report presented here is not in agreement with the results reported by Katayon *et al.* (2004), who noted a decrease in turbidity removal efficiency of MO extracts stored longer than a day. This may be attributed to the difference in protein compounds in okra and MO seeds, because many proteins can be denatured within a few hours of storage. Here, the degradation in performance after the tenth day was caused by the aggregation, precipitation and repugnant odour emission from the protein sample. It was observed during the course of the study that, there was also the issue of physical protein agglomeration and adhesion on the container which could have added to the degraded performance after the tenth day. A wide range of characteristics can be exhibited by denatured proteins, from reduced solubility to communal aggregation.

OSEX was also heated (and so denatured) at different temperatures and its coagulation efficiency evaluated after the heat treatment as shown in Figure 6. It was observed that at the lower coagulant dose of 10 mg/l, the efficiencies of the heat-treated samples deteriorated compared to the native sample. This could be due to the disruption of both the secondary and tertiary structure of the proteins with only the primary structure available for activity which might have low coagulation potential at a lower dose. However, there were improvements in coagulation efficiencies at all doses above 10 mg/l. The highest performances were recorded at 80 mg/l for all the coagulants but the heated samples showed more than a 97% reduction in turbidity compared to 93% for untreated sample (native). It was further observed that the degree of improvement was rather varied across the denatured samples at doses of (20–60 mg/l) but still recorded approximately the same efficiency at 80 mg/l. Thus, heating can improve the coagulation potential of okra crude extract for people in developing countries as home water treatment coagulant, where access to clean water is a big challenge. At a coagulant dose of 100 mg/l, all the samples deteriorated in performance compared to 80 mg/l. It is noteworthy that the deteriorated performance of the denatured samples still outperformed the highest recorded efficiency of the non-denatured sample. This shows that the extract is stable after heat treatment. Again, it was seen that heating could improve the effectiveness of the filtration process. The time taken to filter 100 ml of the heated sample was between 30 and 40 minutes compared to more than 6 hours for non-treated sample. This demonstrates that the denaturation of proteins that are partially sensitive to storage time and temperature are beneficial, since their removal during the process further improves the quality of the coagulant protein. The two processes can therefore be considered as a simple protein purification technology which can easily be adopted in developing countries.

An assessment of the performance of the denatured sample on a very high turbidity water of 550 NTU was undertaken. Figure 7 shows the removal of turbidity was found to be more than 99% with a residual turbidity of 2.7 NTU at optimum coagulant dose of 200 mg/l. This is similar to river water turbidity found in most tropical countries of the world, especially after heavy rainfall. Therefore, a higher coagulant dose may be required to achieve the WHO water quality standard as shown in this experiment.

Further work is required to assess the potential of treating natural water which may contain natural organic matter as contaminants with okra extract.

The antibacterial activity of the denatured OSEX and alum was tested on contaminated river water with low turbidity level (spiked with kaolin), using collilert-18 Quanti-Tray method. The Quanti-Tray test was conducted to assess the bacterial removal efficiency of the extract. The result revealed that at coagulant doses of 50 and 80 mg/l, the total *E. coli* count in the water was reduced by 89% and 93%, respectively, but the coliform counts remained unaffected after the test, as shown in Table 1. On the other hand, when alum was used as coagulant, total *E. coli* count in the water was reduced by 86% while there was also a 28% reduction in total coliform count. It is clear here that the reduction in *E. coli* in OSEX treated water was due to inactivation capability of the extract. Again the results revealed that some of the organic compounds in the seed can serve as substrates to many pathogens in the water which feed on it and hence remain unaffected during the treatment. This result shows that *E. coli* are more sensitive to the chemical compounds in the extract than the other microbes in the water. Madsen *et al.* (1987) had shown a direct relationship between *E. coli* reduction and removal of turbidity in treated water with MO extract at optimal coagulant dose. The okra seed contains phenol, alkaloids, flavonoids, saponins and ribosome-inactivation proteins (Kondo & Yoshikawa 2007) which show clearly that the extract has pathogen inactivation capability. Another possible reason for the reduction in *E. coli* count could be due to bacterial attachment to the floc during sedimentation as reported by Madsen *et al.* (1987). Furthermore, turbidity removal was 88% at optimum coagulant dose of 50 mg/l while at a higher dose of 80 mg/l, turbidity removal was only 75% with OSEX whereas alum achieved up to 98% reduction in turbidity in the water after treatment. It can be deduced from the study that the coagulation mechanism was the main cause of *E. coli* count reduction in alum treated water, while the reduction achieved with the extract was due to inactivation potential of OSEX as a coagulant since the coliform count remain unaffected after treatment.

The different protein bands in crude extract (Figure 8, lane 1) and denatured samples of okra (by heating – lanes 2 and 4, at 140 and 60 °C, respectively) and storage (lane 3) were compared in order to assess the effect of heat treatment and storage time on protein denaturation. The results show

that the band in the CE with MW of 15 kDa was removed following heat treatment and was faint and less dense in the stored sample, indicating its susceptibility to heating and storage. The concentration of the band between 17 and 21 kDa was more discernible in the heat-treated samples than in the crude extract and stored samples. This indicates many overlapping protein compounds that were removed during heating and prompted the increase in coagulation efficiency. It is clear that the wider and denser band of proteins around 43 kDa in the heated samples was as a result of the effectiveness of the heat treatment. This facilitated the removal of the overlapping proteins in the band that possessed non-coagulating compounds. It is thought that these are the reasons why there was increased coagulation activity in the heat-treated sample compared with the crude extract. It is also believed that the presence of a protein-protein complex could hinder coagulation activity. Bodlund *et al.* (2014) also showed in a study where some mustard seed species were heated at 95 °C for 5 hours and observed the mustard seeds to be thermo-stable, which resulted in increased coagulation performances of the extracts. It was observed in this study that heating and proper storage of the extract samples before employing in water treatment can effectively remove the coagulation-hindering protein in the seed for effective performance.

CONCLUSION

Denaturing the protein of okra seed either by heating or storage destroyed both the secondary and tertiary structure of the protein, yielded an increase in MW of 21 and 43 kDa and gave rise to improved coagulation performance. Denaturing is, therefore, considered advantageous to people in developing countries where access to clean drinking water is still a major cause of health problems, though the increase was not much.

The crude extract sample of okra seed showed high coagulation activity in high turbidity water than in low turbidity water. Although not as effective or efficient as the denatured samples, it can still be considered as a good coagulant in terms of turbidity removal in home water treatment.

The bacterial inactivation capability of the extract is notable, eliminating *E. coli* by approximately 89% at optimum

dose and 93% with a higher dosage, thought to be due to the presence of saponins and ribosome-inactivating protein in the extract. Further tests on its minimum inhibitory concentration on *E. coli* and other pathogenic bacteria found in water are required to reveal its further potential as a disinfectant.

Okra extract quality can be improved locally by simple heat treatment at household level without any requirement for more sophisticated heating facilities to achieve the desired improvement in treated water quality.

FUNDING

The first author appreciates and remains grateful to the Tertiary Education Trust Fund (TETFund AST & D/2013/14) and Nigerian government for funding this research work.

ACKNOWLEDGEMENTS

The authors wish to acknowledge the assistance in the laboratory work given by Mr Mark Carter of the School of Civil Engineering, University of Birmingham, UK.

CONFLICT OF INTEREST

The authors wish to declare that there are no conflicts of interest regarding the publication of this paper. The present research work was not financially supported by any person or organisations since the beginning to the end of this submitted work that may have any influence whatsoever on this paper.

AUTHORS' CONTRIBUTIONS

The first author conducted the laboratory experiments and participated in the analysis of the results and writing up of the paper. The second author participated in reviewing the experimental procedures, results analysis and writing the paper.

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