

## Cavity length downstream of a sudden fall-expansion aerator in chute

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### ABSTRACT

Cavity length has been proven to have a significant effect on the air entrainment of an aerator in flood discharge engineering; however, the estimation of both the bottom and lateral cavity lengths downstream of a sudden fall-expansion aerator remain unclear. This research conducts a series of experiments involving various approach-flow conditions and geometric parameters of an aerator. An improved solution of the cavity length for the bottom and lateral cavities is established. The proposed equation was validated through the data of experiments and predecessor formulas, and exhibited a higher precision than other methods. Both the transverse turbulence and the axial dynamic pressure are found to be related to the formation of a lateral cavity. The present method involving the lateral cavity length was developed based on dimensional analysis and experimental test. The geometric morphology of a lateral cavity exhibits a parabolic shape, which is similar to that of the bottom cavity.

**Key words** | cavity length, dimensional analysis, experimental, sudden fall-expansion aerator

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### SYMBOL LIST

$a_x, a_y, a_z$	the acceleration along the $x$ -direction, $y$ -direction and $z$ -direction	$K_{1,2}$	the coefficient
$b$	the width of the sudden fall-expansion aerator	$L_{c-jet}$	the length of the lateral cavity length
$C$	the air concentration	$L_{d-jet}$	the length of the bottom cavity length
$C_2, C_{90}$	air concentration of 2% and 90%, respectively	$m$	the weight of control volume
$c_f$	the coefficient of air resistance	$N_{1,2}$	surface tensions
$dB, dh, ds$	the width, thickness, and length of control volume	$p_{1,2}$	pressures in the $x$ -direction
$F$	the transverse force	$p_a, p_c$	the pressures close to the free surface and internal cavity, respectively
$F_a$	buoyancy of the air on a nappe	$P_N$	sub-pressure beneath the cavity
$F_r$	Froude number	$R$	the radius of curvature
$F_r$	air resistance	$R_e$	the Reynolds number (–)
$g$	gravitational acceleration	$t_s$	the drop height of the aerator
$G$	gravity of control volume	$T$	time
$h$	the depth of flow	$u_y$	the lateral diffusion velocity
$H$	the flow depth	$v$	the cross-sectional mean velocity
		$v'$	the fluctuating velocity

$v_0$	the cross-sectional mean velocity at the pressure outlet
$x, y, z$	the horizontal, transverse and vertical coordinates of the nappe profile
$\alpha$	the slopes upstream of the aerator
$\theta$	the slope downstream of the aerator
$\mu$	the dynamic viscosity coefficient
$\sigma$	the coefficient of surface tension
$\phi$	the emergence angle of the flow jet
$\rho_a, \rho_w, \rho_m$	density of the air, water, and air–water mixtures

## INTRODUCTION

Flow aeration by aerators is an inexpensive and effective measure to prevent cavitation erosion in hydraulic engineering (Pfister *et al.* 2011; Hager & Boes 2014). Sudden fall-expansion (vertical drop and lateral enlargement) aerators are frequently adopted in flood discharge tunnels of high-head dams. The cavity length downstream of a sudden fall-expansion aerator includes the bottom cavity length and the lateral cavity length. Cavity length is one of the most important parameters that affect the air entrainment of an aerator (Wu & Ruan 2008; Wu *et al.* 2011; Wu & Ma 2013).

Dimensional concepts complemented with semi-empirical assumptions and simplified theoretical approximations have usually been adopted to estimate the bottom cavity length downstream of a bottom aerator. Those can be divided into four categories: (i) dimensional analysis (Shi *et al.* 1983; Pan & Shao 1986; Xia & Zhang 1999; Mohaghegh & Wu 2009; Pfister & Hager 2010); (ii) projectile theory (Rutschmann & Hager 1990; Ni 1993; Chanson 1995; Yang *et al.* 1996); (iii) the infinitesimal method (Wu & Ruan 2008); and (iv) numerical simulations (Zhang *et al.* 2011; Aghebatie & Hosseini 2016). Most of the methods do not or only partially consider the effect of the exit angle, flow depth, fluctuating velocity and aeration on the bottom cavity length. In terms of the scope of application, most formulas are poor in generality and low in accuracy.

Compared to the bottom cavity, there is little research on the lateral cavity length; this may be because of the unknown mechanism of the formation of the lateral cavity.

A lateral deflector built on the sidewall can increase the cavity length in sudden fall-expansion aerators (Nie *et al.* 2003). These results indicate that the slope of the outlet and the shape of the lateral deflector should be considered in the estimation of the cavity length. Liu *et al.* (2008) proposed that the lateral cavity length was influenced by both the lateral aerator and the bottom aerator. The effects of aerator conformation, the flow velocity and the fluctuating velocity on the lateral cavity were analyzed by Yue *et al.* (2009), Wang *et al.* (2013) and Liu *et al.* (2015). Additionally, some empirical equations have also been established for calculating the lateral cavity length (Yue *et al.* 2009; Liu *et al.* 2015).

Although there are several methods to estimate the cavity length of a bottom aerator or a lateral aerator, few of these methods are suitable for calculating the cavity length downstream of a sudden fall-expansion aerator. A theoretical analysis based on the projectile law and micro-element method was adopted in this study to further the knowledge of cavity length and geometric morphology along the nappe downstream of a sudden fall-expansion aerator on a spillway. The improved expressions were verified through the extensive experimental data from this study and other investigators.

## THEORETICAL CONSIDERATIONS

### Bottom cavity length

The estimation of the bottom cavity length is based on projectile theory. Figure 1 provides a schematic diagram of the jet flow over an aerator. For a control volume of per unit

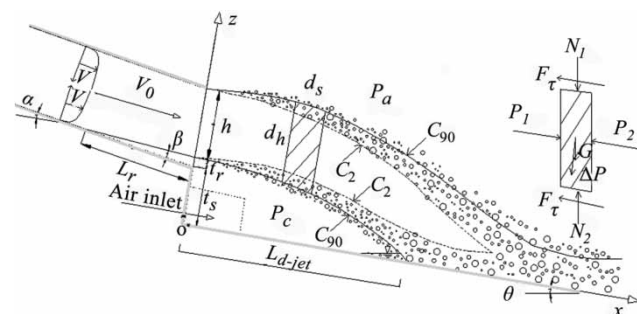


Figure 1 | Sketch of the flow over an aerator.

width (length:  $ds$ , thickness:  $dh$ ): the density of the air–water flow is  $\rho_m = (1 - C)\rho_w + C\rho_a$ , and the weight is  $m = \rho_m dV = \rho_m dhds$ . The forces acting on the control volume include the following:

Gravity:  $G = \rho_m g dhds$

Buoyancy of the air on a nappe:  $F_a = \rho_a g dhds$

Vertical pressures:  $\frac{dh}{h} \Delta p ds = \frac{dh}{h} (p_a - p_c) ds$

Pressures in the  $x$ -direction:  $p_1 \approx p_2$

Vertical surface tensions:  $N_{1,2} = \frac{\sigma}{R} ds$

Air resistance:  $F_r = 0.5c_f \rho_a v^2 ds$

where  $v$  is the cross-sectional mean velocity, approximately equal to the mean velocity ( $v_0$ ) at the pressure-outlet;  $\sigma$  is the coefficient of surface tension ( $\sigma = 0.07275 \text{ Nm}^{-1}$ );  $R$  is the radius of curvature; and  $c_f$  is the coefficient of air resistance,  $c_f = 0.0125$  (Yang et al. 1996).

Among the above-described forces, gravity, buoyant force, pressure, and air drag are the main forces that must be considered, whereas surface tension can be neglected. Then, the expression of the jet trajectory can be written as

$$\begin{cases} \frac{dV_x}{dt} = \frac{(1-C)(\rho_w - \rho_a)}{\rho_m} g \sin \theta - \frac{0.5c_f \rho_a v_0^3}{\rho_m q} \\ \frac{dV_z}{dt} = - \left[ \frac{(1-C)(\rho_w - \rho_a)}{\rho_m} \cos \theta + P_N \right] g \end{cases} \quad (1)$$

where  $P_N = (p_a - p_c)/\rho_w gh$  is the sub-pressure beneath the cavity;  $p_a$  and  $p_c$  are the pressures close to the free surface and internal cavity, respectively; and  $\rho_a$ ,  $\rho_w$  and  $\rho_m$  are the density of the air, water and air–water mixture flow, respectively.

The initial boundary conditions are as follows:

$$\begin{cases} x|_{t=0} = 0, V_x|_{t=0} = v_i \cos \phi \\ z|_{t=0} = t_r + t_s, V_z|_{t=0} = v_i \sin \phi \end{cases} \quad (2)$$

The expression for calculating the bottom cavity length can be obtained by using Equations (1) and (2) as follows:

$$L_{d\text{-jet}} = K_1 T + K_2 T^2 \quad (3)$$

where  $K_1 = v_i \cos \phi$  and  $K_2 = \frac{1}{2} \left( \frac{(1-C)(\rho_w - \rho_a)}{\rho_m} g \sin \theta - \frac{0.5c_f \rho_a v_0^3}{\rho_m q} \right)$ . The flow jet was assumed to be formed

by a solid particle, and its flight time  $T$  was defined as

$$T = \frac{v_i \sin \phi}{\left( \frac{(1-C)(\rho_w - \rho_a)}{\rho_m} \cos \theta + P_N \right) g} \left( 1 + \sqrt{1 + 2g(t_r + t_s) \left( \frac{(1-C)(\rho_w - \rho_a)}{\rho_m} \cos \theta + P_N \right) / (v_i \sin \phi)^2} \right)$$

and  $v_i$  can be calculated by modifying the mean velocity at the pressure outlet as  $v_i = \sqrt{v_0^2 + v'^2}$ , where  $v_0$  is the mean velocity. Based on the results of Pope (2000), the fluctuating

velocity  $v'$  can be calculated as  $v' = \frac{v_0}{5 \log_{10}(2v_0 h_0 / \nu) - 2.4}$ ,

where  $\nu = 1.01 \times 10^{-6} \text{ m}^2 \text{ s}^{-1}$  is the kinematic viscosity coefficient,  $C$  is the mean air concentration, and  $\phi$  is the emergence angle of the jet. According to the present experiments and the results of Wu & Ruan (2008), an improved expression for the emergence angle is given as

$\phi = \beta \sqrt{\tanh\left(\frac{t_r}{h_0 \beta} e^{\frac{2.7725}{t_r - 1}}\right) + (\theta - \alpha) - \arctan\frac{v'}{v_0}}$ ;  $\theta$  is the angle with respect to the horizontal;  $g$  is the acceleration of gravity.

The trajectory equations of the lower nappe can be expressed as

$$\begin{cases} x = (v_i \cos \phi)t + \frac{1}{2} \left( \frac{(1-C)(\rho_w - \rho_a)}{\rho_m} g \sin \theta - \frac{0.5c_f \rho_a v_0^3}{\rho_m q} \right) t^2 \\ z = (v_i \sin \phi)t - \frac{1}{2} \left( \frac{(1-C)(\rho_w - \rho_a)}{\rho_m} \cos \theta + P_N \right) g t^2 + (t_r + t_s) \end{cases} \quad (4)$$

The overall factors that affect the bottom cavity length, including the aeration, the cavity pressure, the emergence angle and the aerodynamic drag, were considered in Equations (3) and (4).

**Lateral cavity length**

As is generally known, hydrodynamic pressure is always generated when water flows in a pressure-tunnel. The cross-sectional distribution of hydrodynamic pressure is that it is higher near the center and lower near the circumference (Ai & Shen 1995). The water cannot diffuse because of the restriction of the surrounding wall. When the water flow arrives at the sudden fall-expansion aerator, the pressure around the water surface immediately changes to atmospheric pressure whereas the hydrodynamic pressure inside the water remains high. The internal high pressure must inevitably spread to the surrounding water-free surfaces, resulting in the water spreading. Additionally, the high-speed water within the intense turbulence and the Reynolds stress can affect the transverse diffusion flow too (Ghasemi et al. 2015). The two factors mentioned can be integrated and expressed as a transverse force  $F$  that results in the formation of the side cavity.

Figure 2 is the schematic diagram of the lateral aeration flow. The weight is  $m = \rho_m dV = \rho_m dBds$  for a control volume of unit height (width  $dB$  and length  $ds$ ). The forces acting on the control volume include the following:

Side surface tensions:  $N_1 = \frac{\sigma}{R} ds$

Air resistance:  $F_r = 0.5c_{fr}\rho_a v^2 ds$

Pressures in the  $x$ -direction:  $p_1 \approx p_2$

Transverse force:  $F$

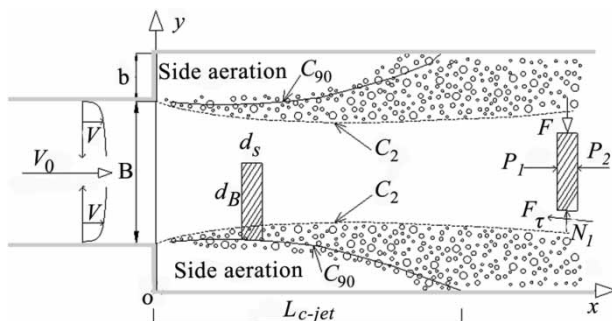


Figure 2 | Flow pattern of the aerator with lateral enlargement.

The definitions of the symbols are the same as those noted above.

Under the conditions in this test, the air resistance of the lateral nappe is approximately 0.002418–0.0054 N, which is a microscopic force that can be ignored. Analogous to the aforementioned analysis of the lower nappe, the trajectory of the lateral nappe ( $x$ - $y$  coordinates) can be written as

$$\begin{cases} x = v_0 t \\ y = -0.5a_y t^2 + u_y t + b \end{cases} \quad (5)$$

where  $a_y$  is the acceleration along the transverse direction,  $u_y$  is the lateral diffusion velocity, and  $b$  represents the width of the lateral expansion.

Then, the trajectory of the lateral nappe can be expressed in the following form:

$$y = -\frac{a_y}{2v_0^2} x^2 + \frac{u_y}{v_0} x + b \quad (6)$$

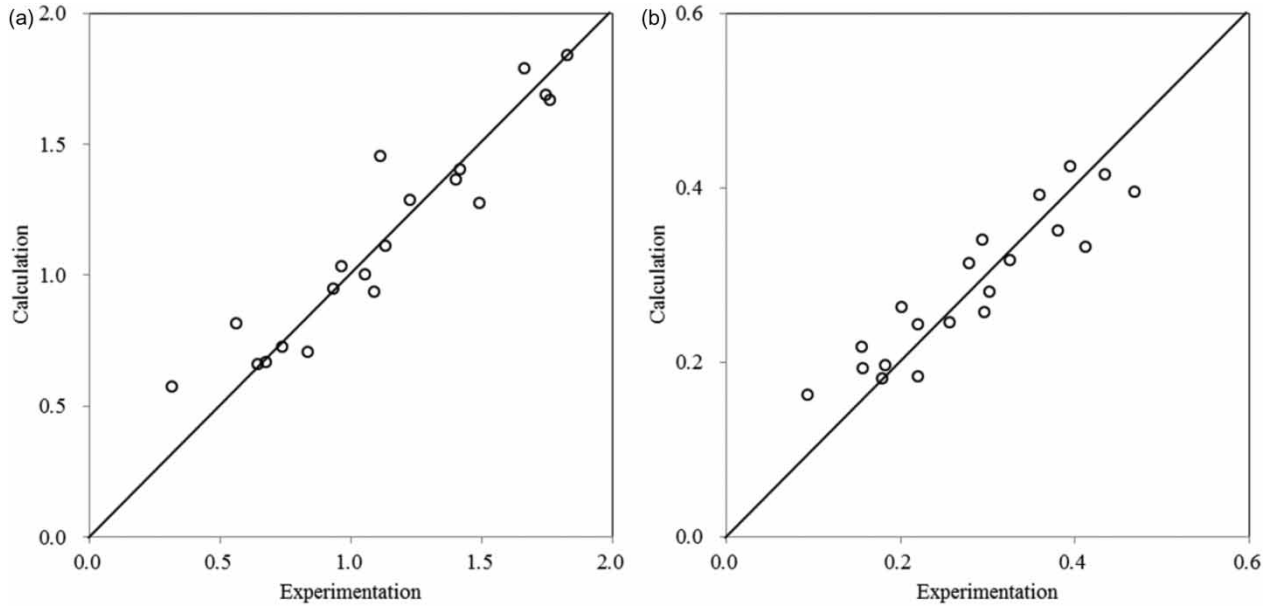
The lateral cavity length can be expressed as

$$L_{c-jet} = v_0 T = v_0 \frac{u_y + \sqrt{u_y^2 + 2a_y b}}{a_y} \quad (7)$$

Equation (7) is derived from Equation (5), including two main parameters ( $u_y$  and  $a_y$ ), which are crucial to determining the cavity length. A dimensional analysis was performed to determine those two parameters in this research.

Based on the present experiments and the previous studies, the lateral cavity length is considerably influenced by the following factors: (1) the bottom slopes upstream ( $\alpha$ ) and downstream ( $\theta$ ) of the aerator, the lateral width  $b$  and the drop height  $t_s$ ; (2) the flow velocity  $v_0$  and the depth  $h$ ; (3) the pressure in the lateral cavity  $p'_c$  and the gravitational acceleration  $g$ ; and (4) the density of air–water  $\rho_m$ , the dynamic viscosity coefficient  $\mu$ , and the surface tension  $\sigma$ . In this study, the Reynolds number is approximately  $(0.89-1.24) \times 10^6$ , which is large enough to ignore the viscous force. There is no negative pressure in the lateral cavity because of good ventilation conditions. The surface tension has less effect on a high velocity flow. Then, the dimensional analysis of the cavity length yields

$$L_{c-jet} = f(h, g, \rho_m, v_0, b, t_s, \alpha, \theta) \quad (8)$$



**Figure 3** | Comparison of the experimental data and calculation results: (a)  $a_y/g$ ; (b)  $u_y/(gh)^{0.5}$ .

The independent dimensions  $h$ ,  $\rho_m$  and  $g$ , which include [L], [T] and [M], were employed in the present dimensional analysis, namely,  $[h] = [L^1T^0M^0]$ ,  $[g] = [L^1T^{-2}M^0]$  and  $[\rho_m] = [L^{-3}T^0M^1]$ . The remaining variables can be represented by the three basic dimensions as follows:

$$\pi = \frac{L_{c-jet}}{h^x g^y \rho_m^z}; \quad \pi_1 = \frac{v}{h^{x_1} g^{y_1} \rho_m^{z_1}}; \quad \pi_2 = \frac{b}{h^{x_2} g^{y_2} \rho_m^{z_2}}; \quad \pi_3 = \frac{h}{h^{x_3} g^{y_3} \rho_m^{z_3}};$$

$$\pi_4 = \alpha; \quad \pi_5 = \theta; \quad \text{and} \quad \pi_6 = \beta.$$

According to the principle of dimensional harmony, the exponents are determined as follows:  $x = 1$ ,  $y = 0$  and  $z = 0$

$$\text{for } \pi = \frac{L_{c-jet}}{h^x g^y \rho_m^z}, \text{ namely, } \pi = \frac{L_{c-jet}}{h}. \text{ Similarly, } \pi_1 = \frac{v_0}{\sqrt{gh}} = Fr,$$

$$\pi_2 = \frac{b}{h} \text{ and } \pi_3 = \frac{t_s}{h}.$$

Then, the expression for calculating the lateral cavity length is as follows:

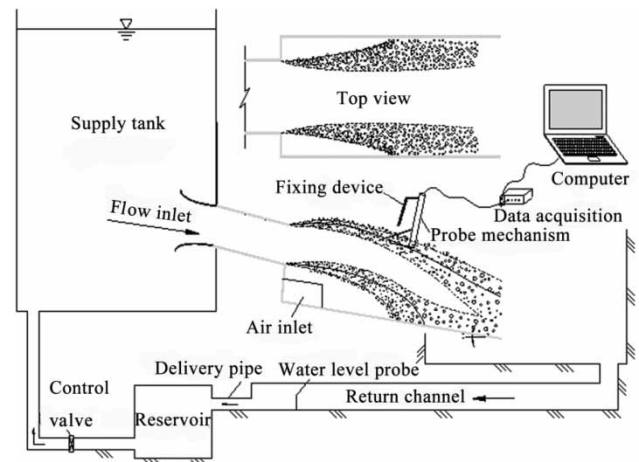
$$\frac{L_{c-jet}}{h} = F\left(\frac{v_0}{\sqrt{gh}}, \frac{b}{h}, \frac{t_s}{h}, \alpha, \theta\right) \quad (9)$$

A series of experiments were conducted to determine the parameters in Equation (9). The results indicate a positive correlation between the lateral cavity length and the width of the lateral aerator ( $b$ ), the Froude number ( $Fr$ ), the bottom slopes ( $\theta$ ) and the height of the aerator ( $t_s$ ).

Therefore, those parameters are summarized in the dimensionless parameter  $X^*$ , which can be written as follows:

$$X^* = \left(\frac{v_0}{\sqrt{gh}}\right)^2 \left(\frac{b}{B+2b}\right)^{0.15} \left(\frac{t_s}{h}\right)^{0.1} (\cos\theta)^{-2} \quad (10)$$

The relationships of the dimensionless acceleration  $a_y/g$  and the dimensionless velocity  $u_y/(gh)^{0.5}$  with  $X^*$  are



**Figure 4** | Schematic of the experimental test equipment.

**Table 1** | Experimental flow conditions

Series	( $t_s, b$ ) / (m,m)	$\theta$	$F_r$	$Re (\times 10^6)$
1	(0.025,0.000)	10%	4.95–7.42	0.89–1.34
2	(0.045,0.000)	10%	4.95–7.42	0.89–1.34
3	(0.065,0.000)	10%	4.95–7.42	0.89–1.34
4	(0.000,0.025)	10%	4.95–7.42	0.89–1.34
5	(0.000,0.045)	10%	4.95–7.42	0.89–1.34
6	(0.000,0.065)	10%	4.95–7.42	0.89–1.34
7	(0.025,0.025)	10%	4.95–7.42	0.89–1.34
8	(0.045,0.045)	10%	4.95–7.42	0.89–1.34
9	(0.065,0.065)	10%	4.95–7.42	0.89–1.34
10	(0.045,0.045)	0%	4.95–7.42	0.89–1.34
11	(0.000,0.045)	0%	4.95–7.42	0.89–1.34
12	(0.045,0.000)	0%	4.95–7.42	0.89–1.34
13	(0.045,0.045)	25%	4.95–7.42	0.89–1.34
14	(0.000,0.045)	25%	4.95–7.42	0.89–1.34
15	(0.045,0.000)	25%	4.95–7.42	0.89–1.34

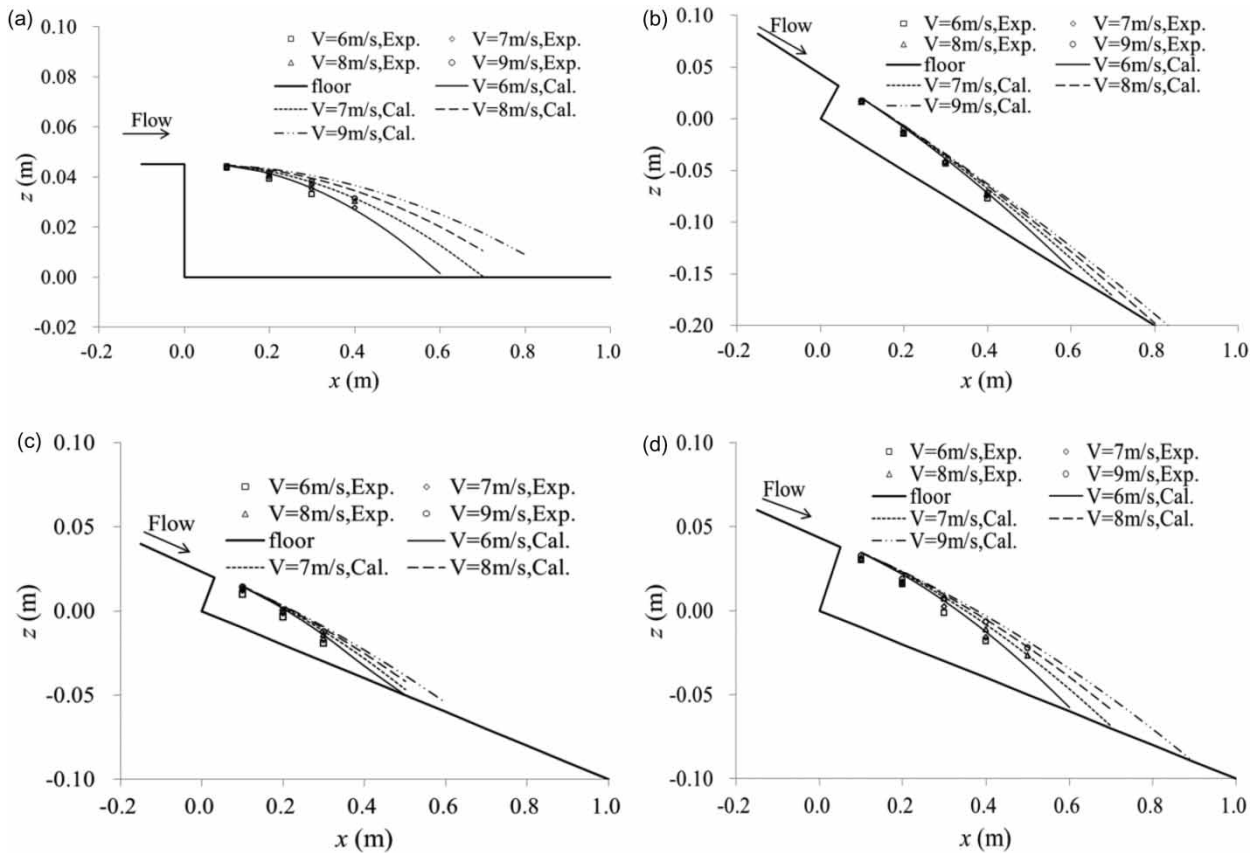
described as follows:

$$\begin{cases} \frac{a_y}{g} = 0.027(X^*)^{1.15} \\ \frac{u_y}{(gh)^{0.5}} = 0.013(X^*)^{0.95} \end{cases} \quad (11)$$

Equation (11) was also tested against the experimental data, and the result is shown in Figure 3. It can be seen that the calculation results agree well with the experimental data.

### VERIFICATION OF THE PRESENT METHOD

The present equations of cavity length were validated through comprehensive experimental tests. Figure 4 shows a schematic of the rectangular flume setup. The experimental parameters are summarized in Table 1. The chute size



**Figure 5** | Comparison of the experimental data with the calculated values of the trajectory of the bottom cavity: (a) ( $t_s, b$ ) = (4.5 cm, 4.5 cm),  $\theta = 0^\circ$ ; (b) ( $t_s, b$ ) = (2.5 cm, 2.5 cm),  $\theta = 25^\circ$ ; (c) ( $t_s, b$ ) = (2.5 cm, 2.5 cm),  $\theta = 10^\circ$ ; (d) ( $t_s, b$ ) = (4.5 cm, 4.5 cm),  $\theta = 10^\circ$ .

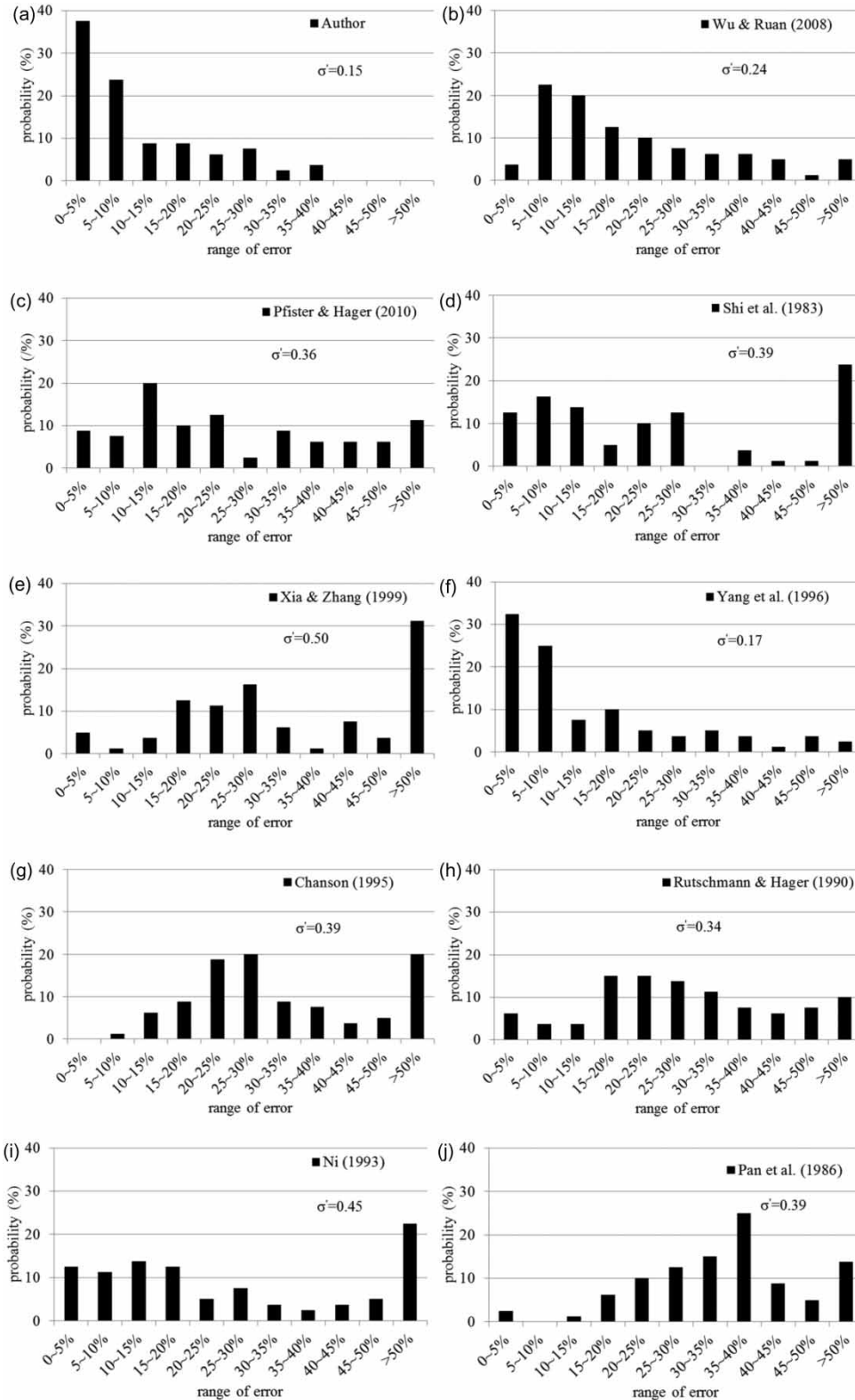


Figure 6 | The relative error of various methods.



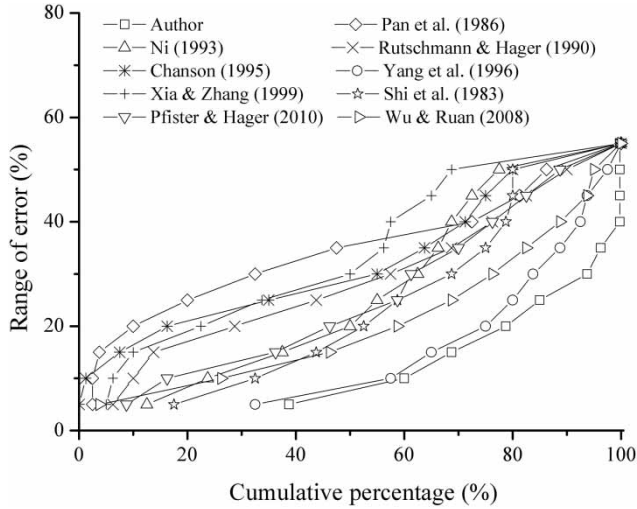


Figure 7 | The cumulative error of various methods.

downstream of the aerator is 3.5 m × 0.3 m × 0.5 m (length × width × height).

The trajectories of the lower nappe (Equation (4)) are used to fit the experimental data. The result proves

the goodness of fit illustrated in Figure 5. The geometric shape of the bottom cavity presents a parabolic distribution. The results also indicated that the present expression has an error of 12%, reflecting the fluctuation of bottom cavity length, caused by the air–water mixture flow.

Equation (3) also fits 80 data from 12 aerators of eight hydropower projects, including Foz do Areia (Pinto et al. 1982), Dongjiang, Lubuge, Fengjiashan, Nuozhadu, Shitouhe, Wujiangdu and Xizhijiang (Ni 1993). Here, the relative error ( $\Delta$ ) between the calculated results ( $L_{\text{calculated}}$ ) and the measured values ( $L_{\text{measured}}$ ), and the root mean square error ( $\sigma'$ ) were adopted (see Equation (12)) to verify the precision of different formulas:

$$\begin{cases} \Delta = (L_{\text{calculated}} - L_{\text{measured}})/L_{\text{measured}} \\ \sigma' = \left( \sum_{i=1}^N [(L_{\text{calculated}} - L_{\text{measured}})/L_{\text{measured}}]^2 / N \right)^{0.5} \end{cases} \quad (12)$$

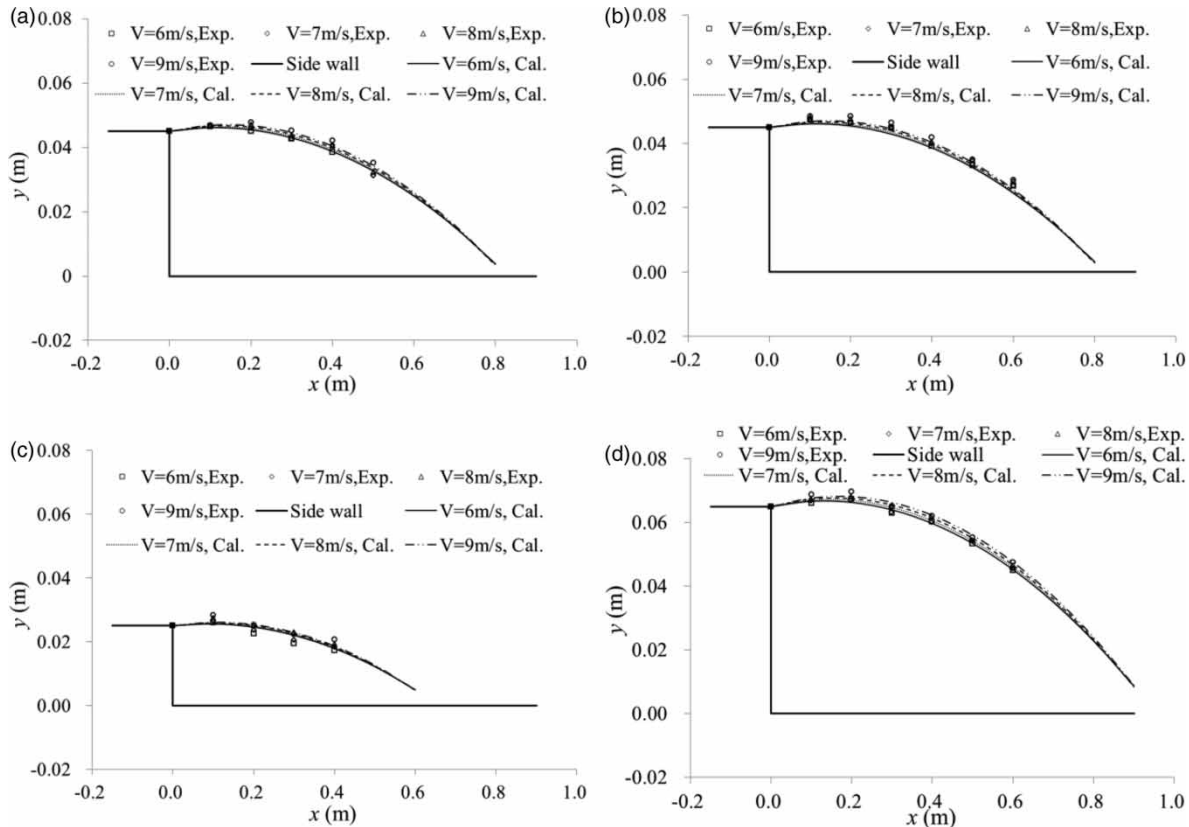


Figure 8 | Comparison of the experimental data with the calculated values of trajectory of the lateral cavity: (a) ( $t_s, b$ ) = (4.5 cm, 4.5 cm),  $\theta = 0^\circ$ ; (b) ( $t_s, b$ ) = (4.5 cm, 4.5 cm),  $\theta = 25^\circ$ ; (c) ( $t_s, b$ ) = (2.5 cm, 2.5 cm),  $\theta = 10^\circ$ ; (d) ( $t_s, b$ ) = (6.5 cm, 6.5 cm),  $\theta = 10^\circ$ .



The root mean square error, the relative error and cumulative error of the formulas are shown in Figures 6 and 7, respectively. Generally, the results demonstrate that the present method has a relative higher accuracy than other methods. The reason may be that this research accounts for more factors which affect the cavity length. It is noted that the accuracy of the method of Yang *et al.* (1996) is slightly lower than the present method. The reason may be that it does not account for the influence of aeration on the cavity.

Equation (7) was also tested against the experimental tests (Figure 8), indicating a good agreement between the predictions and observations. The result shows that the morphology of the lateral cavity obeys a quadratic parabolic curve, caused by the gradually decay of both the internal pressure and the Reynolds stress, which is consistent with the theoretical analysis.

To validate the precision of the equation of lateral cavity length, the data of these experiments and Wang *et al.* (2013) and Liu *et al.* (2015) are plotted in Figure 9. It can be seen that the present calculation results are consistent with the test data. Again, it is proved that Equation (7) can be adopted for calculating the lateral cavity length. Additionally, some discrete data still exist, caused by errors of the

measuring instruments or the different definitions of the cavity length.

## CONCLUSIONS

In this study, the factors affecting the cavity length downstream of a sudden fall-expansion aerator are investigated for various aerator sizes and approach-flow velocities. The following conclusions can be drawn:

- (1) An improved expression for calculating the geometrical morphology and the length of bottom and lateral cavities is established. When compared with other empirical equations, the proposed equation has a higher precision.
- (2) Preliminary analysis of the formation mechanism of the lateral cavity revealed that the lateral cavity is mainly caused by dynamic pressure and transverse turbulent stress. The morphology of the lateral cavity exhibited a quadratic parabolic distribution, which is similar to the curve of the bottom cavity.

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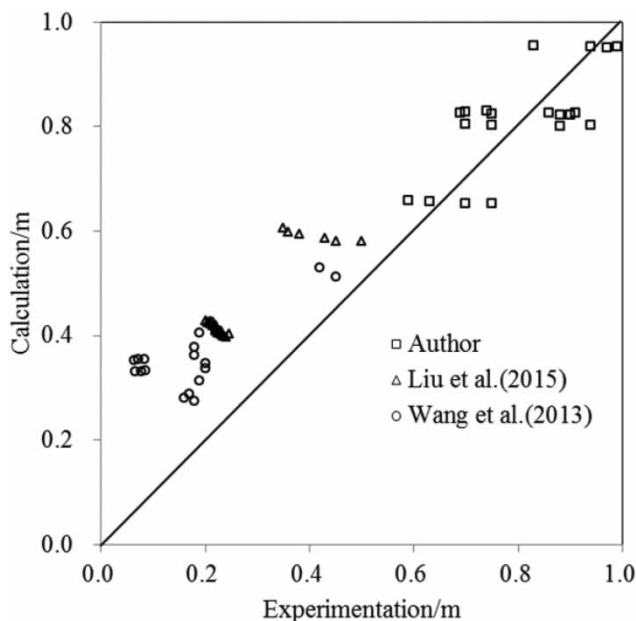


Figure 9 | Comparison of the calculated and experimental data.

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