Use of methyl esterified eggshell membrane for treatment of aqueous solutions contaminated with anionic sulfur dye

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ABSTRACT

The present study assessed the adsorption of an anionic dye (sulfur blue) by methyl-esterified eggshell membrane (MESM), a low-cost and abundant material from waste. Adsorption kinetics were investigated using parameters such as pH, contact time, initial dye concentration, solution temperature, dosage of adsorbent, and particle size of adsorbent. After methyl esterification, the specific surface area significantly increased and the negative surface charge of the eggshell membrane changed to positive for all pH values, which increased the sulfur dye sorption capacity. The optimal conditions for sorption of sulfur dye onto MESM resulted in >98% removal and were as follows: <35 μm particle size, pH 8, 20 min contact time and 313 K temperature. In this respect, 0.68–0.73 dry weight mg/L sulfur dye was adsorbed per 1 mg/L MESM. The Langmuir adsorption capacity for sulfur dye was 187.6 mg/g. In addition, sulfur removal was spontaneous and uptake was endothermic. MESM is an inexpensive and effective adsorbent.

Key words | adsorption, anionic dye, eggshell membrane, kinetics, methyl esterification

INTRODUCTION

The textile dyeing industry consumes around 100–1,100 million tons of various dyestuffs every year in the world and produces large volumes of wastewater including different hazardous chemicals (Choi & Kim 2016). The dyeing wastewater comprises around 2–5% of various dyestuffs and this corresponds to about 2–5 million tons (Işmal et al. 2014). In particular, reactive dyes and sulfur dyes release ca. 20–50% dyestuffs into wastewater through the dyeing process, whereas basic dyes, disperse dyes and acid dyes release ca. 0–5% dyestuffs into wastewater (Nguyen & Juang 2013). Half of the volume of all dyes used on cellulose fibers is sulfur dyes, of which approximately 80% are black sulfur dyes (Ghaly et al. 2014).

The treatment of dyeing wastewater is not easy because dyes are mainly aromatic and heterocyclic compounds. The structure of dyes is complex, stable and not biodegradable in the solution (Ghaly et al. 2014). Thus, the most effective methods and technologies for dye removal involve the adsorption method based on activated carbon. However, this process is costly and the adsorbents are difficult to regenerate after use (Choi & Kim 2016). Therefore, development of a cost-effective, eco-friendly technology for treatment of textile dyeing wastewater is necessary.

The Korean food industry produces 90,000 tons of eggshell waste per year. Of this 26.2% is used as fertilizer, 10.7% as animal feed ingredients, 3.2% for other uses, and the remainder is discarded as waste (Choi & Lee 2016). However, many landfill operators are reluctant to accept eggshell waste because the eggshells and the attached membrane attract pests. Eggshell membrane (ESM) has good adsorbent properties, including the ability to remove heavy metals and dyes from wastewater (Guru & Dash 2014). In general ESM has positively charged at pH 1–6 and negatively charged at pH 6–12 (Chen et al. 2012). The surface property of the ESM dominates its sorption behaviors toward various ions and species. However, the negatively charged carboxylic groups inhibit the adsorption of anion ions by ESM (Tsai et al. 2006). To overcome these problems the ESM surface charge property is changed according to the esterification of carboxylic groups, which is the main driver of improved dye sorption capacity. Methyl-esterified eggshell membrane (MESM) has a high...
cationic charge density and can thus strongly adsorb and destabilize negative particles, such as negatively charged sulfur dyes. MESM from eggshell waste has been recommended for use as an adsorbent because of its low cost, copious availability, non-toxicity, high specific surface area, biodegradability, high potential for ion exchange for charged pollutants, and safe handling (Chen et al. 2015). Moreover, MESM can be regenerated and reused several times. Biological, chemical, and physical processes for heavy metal removal using eggshell (Rohaizar et al. 2013; Pettinato et al. 2015) and ESM (Chen et al. 2012, 2015) have been reported. However, no examination of MESM for removal of sulfur dyes has been reported. Therefore, the novelty of this study is its proposal of effective use of MESM for removal of sulfur dye from aqueous solution. We expect MESM to be used as an eco-friendly adsorbent in place of other chemical dye-removal agents.

**MATERIALS AND METHODS**

**Materials**

Waste eggshell samples were collected from a chicken farm in Gangneung City, Korea. To remove all adhering and interfering materials, such as organics and salts, the samples were rinsed several times with deionized water and then boiled in water. After cleaning, the eggshells were dried in an oven at 80 °C for 24 h. The dried eggshells were first pre-treated with 15% (v/v) HCl overnight to dissolve the outer layer of the shell and leave the ESM. The separated ESM was then cleaned using deionized water, dried at 80 °C for 24 h in an oven, and crushed into fine powder using a mortar and pestle for future use. Thereafter, 100 mg of the pretreated ESM powder was immersed in 50 mL methanol containing 2% (v/v) HCl for 10 h at 80 °C to esterify carboxylic groups in the ESM structure. The resultant MESM was rinsed several times with deionized water, dried at 80 °C for 24 h in an oven, and stored in a desiccator for future use.

Sulfur blue 11 (CI 53235 and molecular weight 305 g/mol; Tera Pharmaceuticals Inc., Buena Park, USA) was used as anionic dye for adsorption onto ESM and MESM. The sulfur dyes were adsorbed by cotton from a bath containing sulfide and insolubilized within the fiber by oxidation (Ding et al. 2010). Therefore in this study, the water-soluble form of sulfur blue was generated by alkaline reduction with sodium sulfide.

**Experimental design**

The sulfur dye removal onto MESM was investigated using various parameters, such as particle size, pH and temperature. In addition adsorption kinetics using a pseudo-second-order model, adsorption isotherm using Langmuir and Freundlich, and adsorption thermodynamics were analyzed. The experiment was carried out in the form of a batch-test. For the effect of MESM on sulfur dye removal, an MESM particle size of 20–100 μm, initial sulfur dye concentration of 1–40 mg/L, and MESM doses of 1–30 mg/L were added in various concentrations of sulfur dye containing in 1 L water. The suspension was shaken for various lengths of time (1–120 min) with controlled pH. The pH was controlled from 1 to 12 using NaOH and/or H₂SO₄, and a temperature range of 283–315 K was used to assess the effect of temperature. Defined amounts of MESM were added to aqueous solutions of sulfur blue, and the suspension was shaken for varying lengths of time. At the end of the run, the suspension was centrifuged at 1,500 rpm (628 g) for 20 min. Supernatant was removed at predetermined time points from the middle of the dye suspension and filtered through a 0.45 μm membrane filter (Watman, Sigma-Aldrich) to separate the filtrate and adsorbent residue. All experiments were carried out by changing one parameter at a time while holding the others constant.

**Analytical methods**

The Brunauer–Emmett–Teller (BET) surface area of the samples was determined using a Protech Korea BET surface area analyzer (Model ASAP 2020). The particle size and amount of sericite were analyzed using laser diffraction (Laser Diffraction Master Class 3&4, Malvern, UK) and micro scales (XP26, Mettler Toledo, Switzerland), respectively. Zeta potential measurements of ESM and MESM in aqueous solution were conducted using a Malvern Zetasizer nano-Z analyzer (Malvern, UK). A scanning electron microscope (SM-300, Topcon, Japan) with an energy dispersive spectroscopy (EDS spectrometer, Shimadzu, Japan) was used for surface imaging and elemental analysis of MESM and ESM. The point of zero charge (PZC) of the adsorbent was determined by the solid addition method. A detailed measurement method of PZC is given in the literature (Bertolini et al. 2013). The absorbance of filtered samples was measured at the peak wavelength of dye (λmax sulfur blue = 620 nm) using a UV-2550 UV-visible spectrophotometer (Shimadzu, Japan). The adsorption capacity was
calculated using the equation below:

\[ q_e = \frac{[(C_0 - C_e)V]}{m} \]  \hspace{1cm} (1)

where \( q_e \) (mg/g) is the adsorption capacity, the dye uptake by a unit weight of adsorbent; \( C_0 \) (mg/L) is the initial concentration of dye; \( C_e \) (mg/L) is the residual concentration; \( V \) (L) is the volume of solution and \( m \) (g) is the weight of adsorbent.

Removal efficiency (%) was calculated to investigate the percentage of dye removal as follows:

\[ R = \left\{ \frac{(C_0 - C_e)}{C_0} \right\} \times 100\% \]  \hspace{1cm} (2)

where \( R \) (%) is the removal ratio, \( C_0 \) (mg/L) is the initial concentration of dye and \( C_e \) (mg/L) is the residual concentration of dye. The high cationic charge density of MESM allows it to strongly adsorb the negatively charged regions of sulfur dyes. All experiments were repeated five times, and average results are presented.

RESULTS AND DISCUSSION

**Characterization of ESM and MESM**

Scanning electron microscopic (SEM) images of ESM samples before and after methyl esterification are shown in Figure 1(a) and 1(b), respectively. The SEM images of ESM and MESM demonstrate similar morphologies. MESM has a porous structure similar to ESM; however, it is composed of a network of fibrous proteins, such as collagen type, (Figure 1), and the specific surface area was increased which would enable adsorption of the sulfur dye in aqueous solution. ESM contains various organic/inorganic matter and minerals. Chen et al. (2015) reported that the C, N, and S contents in ESM were 42.6, 31.5, and 9.9%, respectively. In this study after methyl esterification, the contents of C, N and S were determined as 54.7, 20.4, and 7.4%, respectively. The increase in C and decreases in N and S further indicated the esterification of carboxylic groups on the ESM surface.

The BET specific surface area, pore volume and pore size for ESM and MESM are shown in Table 1. The pore size and pore volume of ESM were significantly increased after methyl esterification. Moreover, the activation caused a marked increase in specific surface area from 4.45 to 57.62 m²/g.

The PZC is defined as the pH at which the surface of the adsorbent has neutral charge. The pH_pzc adsorbents depend on several factors such as the nature of crystallinity, impurity content, temperature, adsorption efficiency of electrolytes, and degree of adsorption of H⁺ and OH⁻ (Appel et al. 2003). At pH = pH_pzc sulfur dye was adsorbed on ESM even though the surface charge was neutral, indicating the sulfur dye was adsorbed by other mechanisms than electrostatic attraction. The value of pH_pzc of ESM was lower than the pH in water indicating that the surface presented a negative charge in aqueous solution (pH > pH_pzc). The value of the pH_pzc of ESM obtained in this study was 6.3 (Table 2). The value is lower than the pH and the surface of ESM also showed negative charge.

ESM and MESM surfaces are shown in Figure 2. The ESM surface was positively charged at pH 1–6 and negatively charged at pH > 6. However, MESM was positively charged over the entire pH range. The potential of MESM was...
5–10 mV at all pH values, whereas that of ESM varied from 23.7 to –16.2 mV over all pH values and changed significantly at pH 6. The negatively charged carboxylic groups present on ESM inhibit the adsorption of anion species (Nguyen & Juang 2016). After methyl esterification, the negative surface charge property of ESM is changed to positive at all pH values, which improves the sulfur dye sorption capacity. In general, potential values of ±5 mV represent rapid adsorption, while values from ±10 to ±30 mV represent unstable adsorption (Choi 2015). In this study, the MESM potential for all pH ranges was in the range of 0–8 mV.

**Effect of pH**

The pH factor is an important parameter in the dye adsorption process. The pH of an aqueous solution will control the magnitude of electrostatic charges which are imparted by the ionized dye molecules (Choi & Kim 2015). Sulfur dye removal efficiency was determined according to pH (Figure 3). The removal efficiency of sulfur dye by ESM was strongly dependent on pH. The removal rate of sulfur dye by ESM decreased with increasing pH: removal rate of 88 to 70% below pH 6 and 42 to 15% at pH 7–12. In contrast, the removal efficiency of sulfur dye by MESM remained constant at 94–100% at all pH values. This result was related to the pHpzc value of ESM and MESM. The negatively charged surface of ESM exhibited low adsorption of negatively charged sulfur dye up to pH 7. However, positively charged MESM adsorbed a significant quantity of negatively charged sulfur blue. The optimum pH for sulfur dye adsorption by MESM was 5–7. This difference was likely due to the lower anion exchange capacity of ESM. It is interesting to note that anion exchange is restricted to the surface and edges of the ESM particles. In general, the model was able to predict adsorption decay during the very early stages of adsorption. Dye uptake was highly sensitive to pH changes in the adsorption system (Abidi et al. 2013). The adsorption capacity of ESM has been reported previously (Daraei et al. 2015; Rohaizar et al. 2013). The adsorption of metal ions by ESM is strongly dependent upon the conditions. In particular, pH affects binding site protonation, calcium carbonate solubility and metal speciation. To overcome these problems, ESM was esterified with methylene. The adsorption of sulfur dye by MESM was highly effective in the wide range of pH.

**Effect of parameters**

**Effect of particle size range according to contact time**

The particle size of adsorbent is an important parameter for removal of sulfur dye in the aqueous solution using MESM because it significantly depends on the available binding sites of the MESM surface. The adsorption of sulfur blue...
onto MESM is shown in Figure 4(a). Equilibrium was reached in a very short time for all samples. The adsorption capacity decreased with increasing particle size. A particle size range of $<35 \mu m$ resulted in adsorption of 99.38% of sulfur blue onto MESM, compared to 87.5, 75.63 and 69.38% for 36–60, 61–75 and 76–100 $\mu m$ particle size ranges, respectively. This indicated that surface area increases with decreasing MESM particle size for a given mass of MESM; as a consequence the number of binding sites increases. The initial sorption rate also decreased with increasing particle size. This is expected because the external surface area available for reaction decreased with increasing particle size for a constant adsorbent mass. The contact time could influence process performance. An increase in contact time generally enhances sulfur dye removal; however, the ion retro-dissolution phenomenon could take place (Pettinato et al. 2015). As a result, adsorption equilibrium was reached more rapidly with decreasing MESM particle size. However, all MESM particle size ranges achieved adsorption equilibrium in ca. 20 min.

**Effect of MESM dose**

Adsorbent dosage is also an important influencing parameter for the adsorption process. In general, as the quantity of ESM increases, the specific surface area and dye binding sites also increase. However, excessive amounts of the adsorbents may result in particle aggregation, overlapping and overcrowding, resulting in a decrease in surface area and sorption capacity (Pettinato et al. 2015). Therefore, optimization of adsorbent dosage is necessary to reduce the cost and to increase the adsorption capacity. The results indicated that the sulfur dye removal rate increased with increasing MESM dose and sulfur dye removal of 99% was achieved using 10 mg/L MESM (Figure 4(b)). Therefore, approximately 0.68–0.75 dry weight mg/L sulfur dye was adsorbed per 1 mg/L MESM. The most efficient method of dye removal is based on adsorption from solution onto activated carbon. However, this is expensive and the adsorbent is difficult to regenerate after use (Choi 2015). Another efficient method of dye removal is flocculation. Despite its high efficiency, flocculation requires a large quantity of chemicals and high cost. For example, the typical dose of ferric salt required for flocculation was $>500 \text{mg/L}$ (Kim et al. 2015); and the cost of chitosan is $10–1,000 \text{per kilogram}$, depending on the product quality (Mahe et al. 2015). However, MESM is an alternative inorganic adsorbent that has several advantages, including low cost, abundant availability, non-toxicity and high pollutant adsorption capacity. The anion and organic matter adsorption capacity is high because of MESM’s colloidal properties and positively charged layers. Therefore, MESM may represent an alternative environmentally friendly absorbent.

**Effect of temperature**

The temperature dependence of the sorption rate was reflected by the extremely high correlation coefficient (Table 3). The effect of initial sorptive concentration was determined by varying the initial concentration of sulfur...
Adsorption isotherm

The concentration dependence data at equilibrium between MESM and the solution interface were further analyzed using the Langmuir (Equation (3)) and Freundlich (Equation (4)) adsorption isotherm models (Lalhmunsiama & Lee 2016):

\[
\frac{C_e}{q_e} = \frac{1}{(q_0K_L)} + \frac{C_e}{q_0}
\]

(3)

\[
\log q_e = \frac{1}{n}\log C_e + \log K_F
\]

(4)

where \(q_e\) is the amount of solute adsorbed per unit weight of adsorbent (mg/g), \(C_e\) is the equilibrium bulk concentration (mg/L), \(q_0\) is the Langmuir monolayer adsorption capacity (mg/g) and \(K_L\) is the Langmuir constant (L/g). \(K_F\) and \(1/n\) are the Freundlich constants, referring to adsorption capacity and adsorption intensity, respectively. Straight lines with fairly good fits were obtained for the two isotherms; the isotherm constants and the associated \(R^2\) values are shown in Table 3.

The regression coefficients (\(R^2\)) of Langmuir were a better fit than those of the Freundlich adsorption model for sulfur dye removal. The \(K_L\) value increased with increasing temperature. This may be due to the fact that the reaction activity between sulfur dye and MESM was increased with increasing temperature. Therefore, a high temperature is more effective for sulfur dye removal by MESM. Higher values of Langmuir constant and Freundlich sorption capacity obtained may further confirm the strength and affinity of the employed MESM towards the sulfur dye (Lalhmunsiama & Lee 2016). The fractional value of \(1/n\) with the Freundlich isotherm for sulfur dye was \(0 < 1/n < 1\), suggesting that the MESM has a heterogeneous surface structure of active sites. The \(1/n\) value increased within the range of 0–1 with increasing temperature. This means that the Freundlich isotherm becomes more linear with increasing temperature. The Freundlich isotherm is linear if \(1/n = 1\) and, becomes more nonlinear if \(1/n\) decreases (Coles & Yong 2006). Relatively straight lines were obtained between \(C_e/q_e\) versus \(C_e\) for the Langmuir model (Figure 5(a)) and \(\log q_e\) versus \(\log C_e\) for the Freundlich model (Figure 5(b)). This suggests that the interactions of sulfur dye with the MESM surface are chemical in nature.

The Langmuir sorption capacities of various low-cost materials for anionic dye are shown in Table 4. The sorption capacities varied due to differences in the physicochemical properties of adsorbents. MESM has a lower adsorption capacity than microgel or SBA-16. However, MESM has a higher adsorption capacity compared with kaolinite, montmorillonite, and bentonite. In particular, the adsorption capacity of MESM was 1.67- to 4.59-fold higher than that of ESM. MESM has the advantages of use of waste materials, waste recycling and reduction in landfill cost.

Adsorption kinetics

A fast absorption rate and large absorption capacity are important criteria for a better choice of material to be used as a good absorbent. The dynamics of the adsorption can be studied by the kinetics of adsorption in terms of the order of the rate constant (Lalhmunsiama & Lee 2016). In this study pseudo-second-order (Equation (5)) kinetic models were exploited to obtain the sorption kinetics of sulfur dye on MESM. The equations were used in linear form:

\[
\frac{t}{q_t} = \frac{1}{(hq_e^2)} + \frac{t}{q_e}
\]

(5)
where $q_e$ (mg/g) is the maximum sorption capacity, $q_t$ (mg/g) is the amount adsorbed at time $t$, and $k$ (g/(mg min)) is the adsorption rate constant of the pseudo-second-order equation. Linear plots of the $t/q_t$ by $t$ in Figure 5(c) showed the applicability of the pseudo-second-order equation for the sulfur dye with MESM particle of size ranges from $<38$ to $76–100$ μm. The correlation coefficients for the linear plots of $t/q_t$ against time from the pseudo-second-order rate law are greater than 0.994 for all systems for a contact time of 120 min. This result, with the pseudo-second-order model based on the adsorption capacity on the solid phase, suggests that the adsorption of the sulfur dyes onto MESM is controlled by chemisorption involving valence forces through sharing or exchange of electrons between adsorbent and adsorbate (Arshadi et al. 2016).

The calculated parameters for the effect of particle size on and sulfur blue absorption are shown in Table 5. The pseudo-second-order constant ($k$) decreased with increasing particle size and initial concentration and increased with increasing temperature. These data suggest that sulfur blue removal by MESM increased with decreasing particle size and concentration and increasing temperature. The reaction of small MESM particles was more rapid than that of larger particles because the external surface area available

<table>
<thead>
<tr>
<th>Adsorbate</th>
<th>Adsorbent</th>
<th>$q_m$ (mg/g)</th>
<th>Reference</th>
</tr>
</thead>
<tbody>
<tr>
<td>Basic Red 2</td>
<td>SBA-16</td>
<td>240.39</td>
<td>Chaudhuri et al. (2016)</td>
</tr>
<tr>
<td>Basic Red 5</td>
<td>SBA-16</td>
<td>276.24</td>
<td>Chaudhuri et al. (2016)</td>
</tr>
<tr>
<td>Congo red 4BS</td>
<td>Microgel</td>
<td>869.1</td>
<td>Jin et al. (2015)</td>
</tr>
<tr>
<td>Acid red GR</td>
<td>Microgel</td>
<td>1,469.7</td>
<td>Jin et al. (2015)</td>
</tr>
<tr>
<td>Reactive light yellow</td>
<td>Microgel</td>
<td>1,250.9</td>
<td>Jin et al. (2015)</td>
</tr>
<tr>
<td>Sulfur blue</td>
<td>Kaolinite</td>
<td>2.3</td>
<td>Nguyen &amp; Juang (2015)</td>
</tr>
<tr>
<td>Sulfur blue</td>
<td>Montmorillonite</td>
<td>2.6</td>
<td>Nguyen &amp; Juang (2015)</td>
</tr>
<tr>
<td>RR120</td>
<td>Fouchana</td>
<td>9.7</td>
<td>Errais et al. (2011)</td>
</tr>
<tr>
<td>RR120</td>
<td>Bentonite</td>
<td>2.8</td>
<td>Errais et al. (2011)</td>
</tr>
<tr>
<td>Malachite green</td>
<td>ESM</td>
<td>89.72</td>
<td>Chen et al. (2012)</td>
</tr>
<tr>
<td>Organic dye eosin B</td>
<td>ESM</td>
<td>40.9</td>
<td>Ning &amp; Tao (2011)</td>
</tr>
<tr>
<td>Congo Red</td>
<td>ESM</td>
<td>112.3</td>
<td>Liu et al. (2012)</td>
</tr>
<tr>
<td>Sulfur blue</td>
<td>MESM</td>
<td>187.6</td>
<td>Present study</td>
</tr>
</tbody>
</table>

$q_m$: maximum adsorption capacity.
decreased with increasing particle size for a constant sorbent mass. The sorption capacity of MESM increased from 33.33 to 157.89 mg/g as the initial dye concentration increased from 50 to 300 mg/L. The pseudo-second-order equation and regression coefficients for the linear plots were higher than 0.994 for MESM and is shown in Table 5.

Adsorption thermodynamics

The van’t Hoff analysis was used to assess the spontaneity of the adsorption of dyes on MESM:

$$\ln b = \frac{\Delta S}{R} - \frac{\Delta H}{RT}$$

$$\Delta G = \Delta H - T\Delta S$$

where $\Delta H$ is the change in enthalpy (J/mol), $\Delta S$ is the change in entropy (J/(mol K)), $\Delta G$ is the change in Gibbs free energy (J/mol), $b$ is the Langmuir gas constant at temperature T (K) and R is the universal gas constant (8.314 J/(mol K)). The $\Delta S$ and $\Delta H$ values were evaluated from the intercept and slope of the plot of ln $b$ vs. 1/T (Figure 5(d)). The positive $\Delta H$ (29.31 kJ/mol) values suggest that the process is endothermic (Chen et al. 2015) and the positive $\Delta S$ (0.1125 kJ/(mol K)) values reveal an increase in randomness at the solid-solution interface during dye adsorption on the active sites of MESM adsorbent. The $\Delta G$ was $-2.443$, $-3.572$, $-4.705$ and $-5.826$ kJ/mol as the temperature increased to 283, 293, 303 and 313 K, respectively. The decrease of Gibbs free energy with increasing temperature indicates a better adsorption at higher temperature (Singha & Das 2014). Moreover the negative $\Delta G$ values confirm the spontaneous nature of the dye uptake process.

CONCLUSIONS

The carboxyl groups on ESM were esterified with methanol containing 2% (v/v) HCl for 10 h at 80 °C to produce green adsorbent MESM. After esterification the specific surface area significantly increased from 4.45 to 57.62 m²/g and the negative surface charge was changed to positive at all pH values, which improved the sulfur dye sorption capacity. The optimal conditions for sorption of sulfur dye onto MESM (maximum 98% removal) were as follows: <35 μm particle size, pH 8, 20 min contact time and 313 K. Under these conditions, approximately 0.68–0.73 dry weight mg/L sulfur dye was adsorbed per 1 mg/L MESM. Equilibrium sorption data for sulfur dye fitted well to the Langmuir adsorption isotherms and the kinetic data fitted reasonably well to the pseudo-second-order kinetic model. Further, an increase in temperature favored sulfur dye removal, and the sorption process was found to be spontaneous and endothermic in nature. After methyl esterification of ESM, the surface chemistry is more favorable for adsorption of sulfur dyes. Its environmentally friendliness, low dose requirement and high removal efficiency are the advantages of MESM over commonly used adsorbents.

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