

# Efficient removal of three dyes using porous covalent triazine frameworks: adsorption mechanism and role of pore distribution

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## ABSTRACT

Dyes are widely used in production and life. In this study, porous covalent triazine frameworks (CTFs) were synthesized and the adsorption behavior for three dyes was investigated by batch adsorption experiments. CTFs were characterized by various spectroscopic techniques for structure, porosity and surface properties. Several possible adsorption mechanisms were proposed including pore-filling, electrostatic attraction and hydrogen bonding interaction with the triazine structure of CTFs. The mechanisms were further verified by the pore size distribution and pH dependence. Additionally, CTF<sub>DCBP</sub> displayed stronger adsorption affinity and faster adsorption kinetics for dyes, because of the wide pore size distribution. This study provides a new insight into the mesoporous CTFs, which exhibit great potential as an effective adsorbent for dye removal.

**Key words** | adsorption mechanism, covalent triazine framework, dyes, pore size

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## HIGHLIGHTS

- Cation- $\pi$ , hydrogen bond interaction and electrostatic interaction effect were responsible for strong adsorption of dyes to CTFs.
- Mesoporous CTF<sub>DCBP</sub> shows dramatically enhanced adsorption and fast adsorption kinetics for large dyes Chrysophenine G due to the wide pore size distribution, homogeneous and regular-shaped structure.

## INTRODUCTION

Dyes are widely used in various fields, including textile, leather, paper, plating, medicine and food industries etc. (Guo *et al.* 2014; Yu *et al.* 2015; Niu *et al.* 2018; Zhang *et al.* 2018). A large amount of wastewater was produced in the process of production and use, which caused serious environmental pollution and ecological harm (Singh *et al.* 2015; Narvekar *et al.* 2018). In addition, dyes affect the photosynthetic activities of aquatic species due to the color stability, and some of them have high toxicity, carcinogenic, teratogenic and mutagenic effects, and alter gene expression by epigenetic mechanisms (Yao *et al.* 2010; Perullini *et al.* 2014; Ojedokun & Bello 2017; Muthusaravanan *et al.* 2018; Sharavanan *et al.* 2019). Therefore, removal of dyes from wastewater has attracted much attention for decades. Various methods such as adsorption, flocculation, electrochemical,

photocatalysis, advanced oxidation processes and biological methods have been used for treatment of dyes in water solution (Park *et al.* 2012; Sattarahmady *et al.* 2013; Konicki *et al.* 2017; Moreira *et al.* 2017; Chen *et al.* 2018; Gu *et al.* 2018; Katheresan *et al.* 2018; Zhao *et al.* 2018).

Adsorption treatment has been recognized as a simple and effective method to remove dyes from aqueous solution, due to its high efficiency, convenience, low cost and easy desorption (Ahmed *et al.* 2020; Navya *et al.* 2020). Many studies have reported the adsorption of dyes on carbon-based materials (Al-Degs *et al.* 2009; Asouhidou *et al.* 2009; Ip *et al.* 2010; Gupta & Khatri 2019; Streit *et al.* 2019; Figueiredo *et al.* 2011). Liu *et al.* reported that ordered mesoporous carbon displayed much stronger adsorption than activated carbon (Liu *et al.* 2009). Gupta & Khatri reported

that the specific area and surface polarity conducted fast and efficient adsorptive removal of organic dyes (Gupta & Khatri 2019). Therefore, carbon-based materials with enlarged pore size avoid the size exclusion effect, leading to relatively high adsorption capacity especially for bulky pollutants.

Covalent triazine-based frameworks (CTFs) were first reported in 2008 (Kuhn *et al.* 2008a). They have attracted great attention for energy gas storage and catalytic support materials (Chan-Thaw *et al.* 2010; Li *et al.* 2018; Jena *et al.* 2018), because of the very large specific surface area, homogeneous pore structure, and high chemical and thermal stability (Kuhn *et al.* 2008a, 2008b; Kuhn *et al.* 2009). We reported that a synthesized CTF showed high adsorption affinity, fast adsorption/desorption kinetics, and complete adsorption reversibility for monoaromatic compounds (Liu *et al.* 2012). In addition, CTFs displayed high adsorption affinity for organic pollutants in previous studies (Liu *et al.* 2012, 2013, 2015, 2017; Zhang *et al.* 2011, 2020). These properties make CTFs a promising adsorbent for the removal of organic contaminants in water treatment. However, to the best of our knowledge, little study has reported the adsorption of dyes on CTFs and the adsorption mechanisms and the role of pore distribution were not well understood.

The objective of this work is to explain the adsorption mechanism for three dyes on CTFs and study the roles of CTF pore structure for adsorption. The synthesized CTFs were characterized by XRD, FTIR and N<sub>2</sub> adsorption/desorption isotherms. Pore size distribution and the effect of pH were further performed to understand the mechanisms.

## EXPERIMENTAL SECTION

### Materials

Methylene blue (MB) and methyl orange (MO) were purchased from Tianjin Institute of Chemical Co., Ltd. Chrysophenine G (CG) was supplied by Tokyo Chemical Industry. 1,4-Dicyanobenzene and 4,4'-biphenyldicarbonitrile were purchased from Aldrich. Chemical structures of MB, MO and CG are presented in Supporting Information (SI) Figure S1.

### Preparation of CTFs

Two different CTFs (named CTF-1 and CTF<sub>DCBP</sub>) were synthesized using monomer 1,4-dicyanobenzene and 4,4'-biphenyldicarbonitrile according to literature method

(Kuhn *et al.* 2008a). The details of the synthesis are listed in SI Text S1 and the structures of CTF-1 and CTF<sub>DCBP</sub> are presented in SI Figure S2.

### Characterization of CTFs

X-ray diffraction (XRD) pattern of CTFs was collected from a RigakuD/max-RA powder diffraction-meter using Cu K $\alpha$  radiation (Rigaku, Japan). Elemental analysis of CTFs was performed in an elemental analyzer of Vario MICRO (Elementar, Germany). Transmission electron microscope (TEM) images of the CTFs were obtained from a JEM-2100 transmission electron microscope. Transmission Fourier transform infrared (FTIR) spectra of the CTFs were measured using a Nexus 870 spectrometer (Nicolet, USA). BET and pore size distribution were obtained on a Micromeritics ASAP 2020 apparatus at -196 °C (Micromeritics Instrument Co., USA).

### Adsorption

Adsorption isotherms were conducted by batch adsorption experiment. Briefly, adsorptions (20 mg of CTF-1 and 10 mg of CTF<sub>DCBP</sub>) were introduced into 40 ml glass vials equipped with polytetrafluoroethylene-lined receiving 40 mL of dyes solution with varied initial concentrations (background solution: 0.02 M NaCl). The samples were mixed using an orbital shaker protected from light at room temperature for 48 h. After filtration, the solute was analyzed using UV-vis spectrometer with detecting wavelengths at 664, 462 and 400 nm for MB, MO and CG, respectively. All adsorption experiments were conducted in duplicate.

Separate sets of experiments were performed to test the effects of pH and ionic strength. In the pH experiments, 10 mg CTF-1 and 40 ml of 50 mg/L MB solution (80 mg/L MO and 12.5 mg/L CG) with different pH was pre-adjusted using 0.1 M HCl and NaOH to ensure the desired pH (3–11) at adsorption equilibrium. In the ionic strength experiments, adsorption was performed using background solutions (0.01, 0.02, 0.05, and 0.1 M) NaCl or CaCl<sub>2</sub> with 10 mg CTF-1 and 40 ml of 90 mg/L MB solution (75 mg/L MO and 20 mg/L CG).

### Pore size distribution of CTFs

The pore size distribution of the adsorbents before and after adsorption were collected by N<sub>2</sub> adsorption/desorption isotherms. The adsorbents after adsorption filtered with

0.45  $\mu\text{m}$  fiber filter and dried at 40 °C using a vacuum drying oven. Prior to determine pore size distribution, the adsorbents (CTF-1 and CTF<sub>DCBP</sub>) were activated at 200 °C, and the adsorbents after loading the dyes were activated at 80 °C.

## RESULTS AND DISCUSSION

### Characterization of CTFs

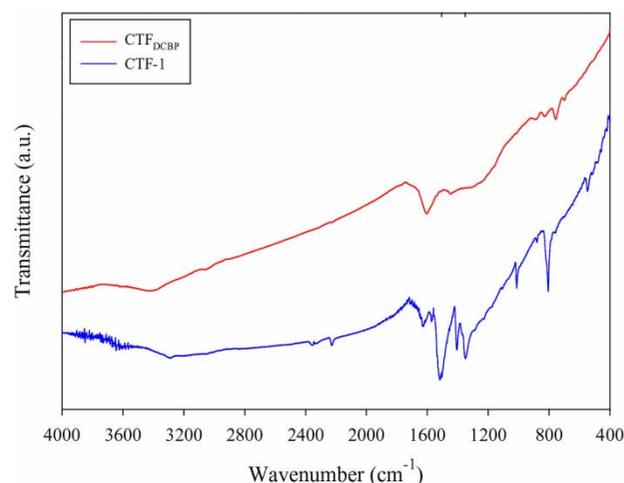
XRD patterns of the CTFs are displayed in SI Figure S3. The diffraction peaks at  $2\theta$  7.2° and 15.1° for CTF-1, reflecting the crystalline triazine-based organic framework with hexagonal pores (Kuhn *et al.* 2008a). Compared with XRD patterns of the CTF-1, CTF<sub>DCBP</sub> showed high disordered crystal because of the salt templating effect (Kuhn *et al.* 2009). Nitrogen adsorption/desorption isotherms of CTFs are presented in SI Figure S4. Obviously, typical capillary condensation was observed within a relative pressure range of 0.2–0.9 for adsorbent of CTF<sub>DCBP</sub>, reflecting the presence of mesoporous. TEM images of CTFs are displayed in SI Figure S5. Similar morphologies are obtained for the CTF-1 and CTF<sub>DCBP</sub>. CTFs presents a homogeneous structure with microporosity, while the structure of CTF<sub>DCBP</sub> becomes rough with increasing mesopore size. BET and pore volume of CTFs are listed in Table 1. The BET surface area of the CTF-1 and CTF<sub>DCBP</sub> were 782.44 and 1,745.45  $\text{m}^2/\text{g}$ , and the pore volume were 0.4 and 1.42  $\text{cm}^3\cdot\text{g}^{-1}$ . In addition, micropores were the major pores of CTF-1, while both micropores and mesopores were detected in CTF<sub>DCBP</sub>. The transmission FTIR spectrum of CTFs is shown in Figure 1. As shown in Figure 1, the strong peaks around 1,352 and 1,507  $\text{cm}^{-1}$  are assigned to vibrations of the triazine structure (Bojdys *et al.* 2010).

**Table 1** | Specific surface area, and total pore volume adsorbents before and after adsorption of methylene blue (MB), methyl orange (MO) and chrysophenine G (CG), on CTF-1 and CTF<sub>DCBP</sub>

CTF-1	Specific surface area <sup>a</sup> ( $\text{m}^2/\text{g}$ )	$v_t^b$ ( $\text{cm}^3/\text{g}$ )	CTF <sub>DCBP</sub>	Specific surface area <sup>a</sup> ( $\text{m}^2/\text{g}$ )	$v_t^b$ ( $\text{cm}^3/\text{g}$ )
Blank	782.0	0.40	Blank	1745.45	1.42
MB	361.35	0.160	MB	602.99	0.476
MO	328.04	0.179	MO	540.77	0.437
CG	642.0	0.316	CG	238.0	0.276

<sup>a</sup>Determined by  $\text{N}_2$  adsorption using the Brunauer-Emmett-Teller (BET) method.

<sup>b</sup>Total pore volume, determined at  $P/P_0 = 0.976$ .



**Figure 1** | Transmission Fourier transform infrared (FTIR) spectrum of covalent triazine-based frameworks.

### Adsorption isotherms

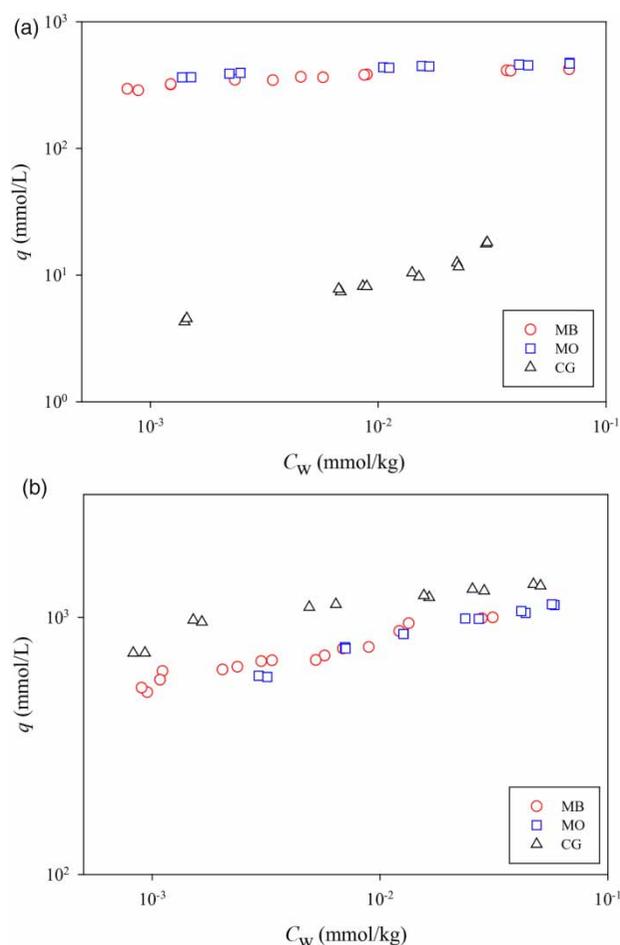
Adsorption isotherms for three dyes on CTFs are presented in Figure 2. Different trends of the adsorption curves between CTF-1 and CTF<sub>DCBP</sub> are observed in Figure 2. Adsorption of dyes on the CTF-1 is ordered as follows: MB  $\approx$  MO > CG. The adsorbent-to-solution distribution coefficient ( $K_d$ ) on CTF-1 was  $10^3$ – $10^5$  L/kg for MB,  $10^3$ – $10^6$  L/kg for MO, and  $10^2$ – $10^3$  L/kg for CG. However, the adsorption on CTF<sub>DCBP</sub> is ordered as CG > MB  $\approx$  MO. The  $K_d$  value on CTF<sub>DCBP</sub> was  $10^4$ – $10^6$  L/kg for MB,  $10^4$ – $10^6$  L/kg for MO, and  $10^4$ – $10^6$  L/kg for CG. The adsorption data were fitted to the Langmuir and Freundlich model according to Equations (1) and (2):

$$q_e = \frac{q_m b C_e}{1 + b C_e} \quad (1)$$

$$q_e = K_F C_e^{1/n} \quad (2)$$

where  $q_e$  (mmol/g) and  $C_e$  (mmol/L) are the adsorbed concentration and the aqueous concentration at adsorption equilibrium,  $q_m$  (mmol/g) is the adsorption capacity, and  $b$  (L/mmol) is the Langmuir affinity coefficient,  $K_F$  ( $\text{mg}^{1-n} \text{L}^n/\text{g}$ ) is the Freundlich affinity coefficient;  $n$  is the Freundlich linearity index. The fitting parameters are summarized in SI Table S2. Adsorption of three dyes to the CTFs can be well described by the Freundlich model with  $R^2$  higher than 0.93. In addition, the linearity indexes ( $n$ ) are smaller than 1, suggesting adsorption heterogeneity.

The cavity of CTF is composed of benzene rings and triazine rings that form a large conjugated chain



**Figure 2** | Adsorption isotherms plotted as solid-phase concentration ( $q$ ) vs aqueous-phase concentration ( $C_w$ ) at equilibrium for different dyes on CTF-1 (a) and CTF<sub>DCBP</sub> (b).

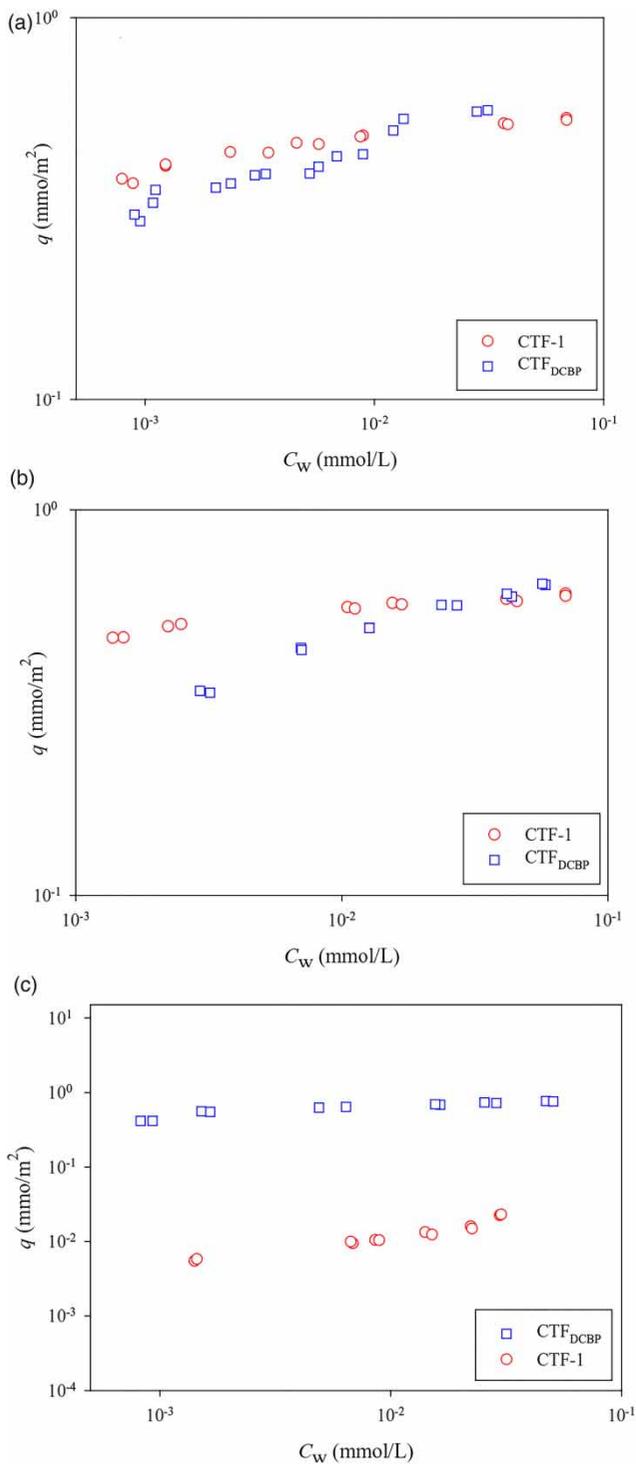
structure, which is rich in  $\pi$  electrons and can be used as  $\pi$ -electron donor (Liu *et al.* 2012). MB as a cationic dye has protonated N atoms. Therefore, cation- $\pi$  interaction mechanism is generated between protonated N in MB and  $\pi$ -electrons in the surface of CTFs, leading to the strong adsorption affinity of MB on CTFs. It is noted that adsorption of MO on CTF-1 and CTF<sub>DCBP</sub> was close to MB, but the adsorption mechanism is different. Electrostatic interaction is likely responsible for the strong adsorption of the dye MO. As shown in SI Figure S6, the point of zero charge (PZC) for CTF-1 and CTF<sub>DCBP</sub> are at pH 7.2 and 8.0. Therefore, the CTFs are positively charged and forming electrostatic interaction with anionic MO. In addition, the triazine structure has a strong ability to form hydrogen bonds, and hydrogen bonding energy between 1,3,5-triazine and water calculation varied from 3.38 to 22.60 kJ·mol<sup>-1</sup> as reported (Li *et al.* 2007). Hydrogen bonding interaction between

polar functional groups and triazine structure further enhanced the adsorption of MO on CTFs. Similar results reported that hydrogen bonds formed between MO and the surface of biopolymer chitin and water/1,2-dichloroethane (Longhinotti *et al.* 1998; Rinuy *et al.* 2000).

Unit surface area-based adsorption data are compared in Figure 3 to further explain the adsorption patterns between CTF-1 and CTF<sub>DCBP</sub>. As shown in Figure 3, adsorption for MB and MO on CTF-1 is higher than on CTF<sub>DCBP</sub>, particularly at low concentration. The strong adsorption for MB and MO on CTF-1 may be caused by the micropore-filling mechanism. Many previous studies (Nguyen *et al.* 2007; Ji *et al.* 2009; Liu *et al.* 2012; Liu *et al.* 2013) have reported this mechanism. Such as Nguyen *et al.* (Nguyen *et al.* 2007) reported that micropore-filling mechanism enhanced aromatic hydrocarbons adsorption on carbonaceous adsorbents. This agrees well with the pore volume results (see SI Table S1). However, adsorption for CG on CTF-1 is dramatically suppressed by the size exclusion effect due to its large molecules. CTF<sub>DCBP</sub> displayed higher normalized adsorption than CTF-1 for CG in Figure 3. This is attributed to the larger mesopore volume of CTF<sub>DCBP</sub>, which effectively avoids the size exclusion effect. The importance of pore structure is further discussed in pore size distribution (see below).

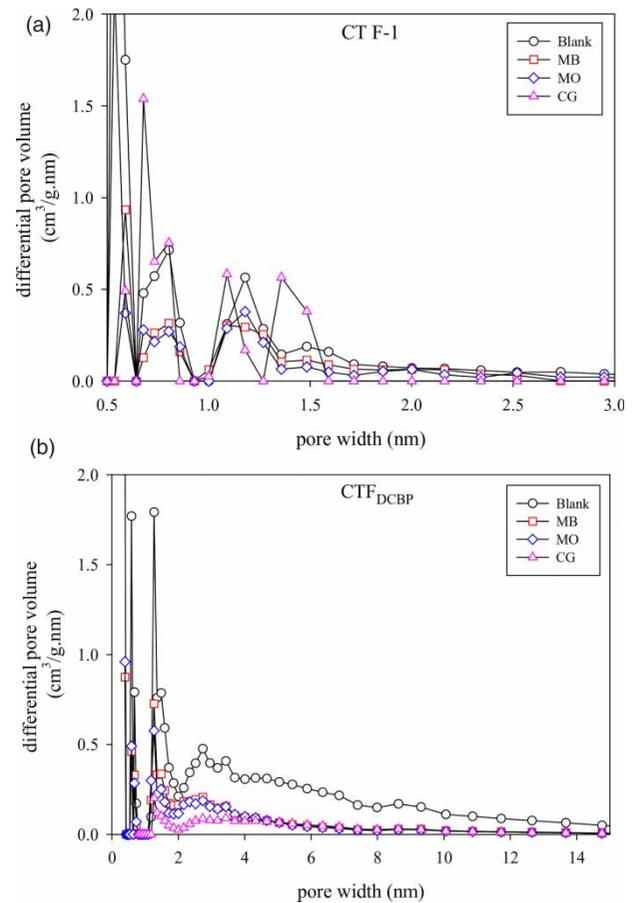
### Pore size distribution of CTFs

Pore size distribution of CTFs before and after dye adsorption are compared in Figure 4 and Table 1 to illustrate the impact of adsorbent pore size and adsorbate molecular size. For CTF-1 in Table 1, the total pore volume of CTF-1 decreased from 0.40 cm<sup>3</sup>/g to 0.160, 0.179 and 0.316 cm<sup>3</sup>/g after adsorption of MB, MO and CG. The slight change of total pore volume for CG is attributed to large size CG, leading to only adsorption on the external surface of CTF-1 because of the size exclusion effect. However, for CTF<sub>DCBP</sub> in Figure 4(b), after adsorption of CG most pore diameters around 2 to 4 nm were shifted significantly and pore volume after adsorption of CG was reduced from 1.42 cm<sup>3</sup>/g to 0.276 cm<sup>3</sup>/g. The strong adsorption for CG on CTF<sub>DCBP</sub> caused by mesopore-filling mechanism due to the size of the CG (size of CG 2.98 nm displayed in Figure S2) matched with the pore width of CTF<sub>DCBP</sub>. It is noted that the total pore volume for MB, MO on CTF<sub>DCBP</sub> also decreased from 1.42 cm<sup>3</sup>/g to 0.476 and 0.437. This indicated that the adsorption sites outside or inside the pores of CTF<sub>DCBP</sub> were occupied efficiently by

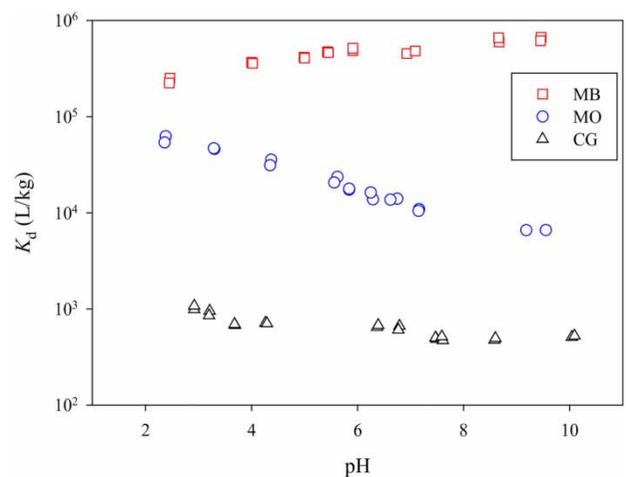


**Figure 3** | Adsorption isotherms of antibiotics plotted as surface area-normalized solid-phase concentration ( $q$ ) vs aqueous-phase concentration ( $C_w$ ) at adsorption equilibrium on CTF-1 and CTF<sub>DCBP</sub>. (a) Methylene blue (MB), (b) methyl orange (MO), (c) Chrysophenine G (CG).

MB and MO, which was attributed to the adsorption mechanisms (cation- $\pi$ , electrostatic interaction and hydrogen bonding) mentioned above.



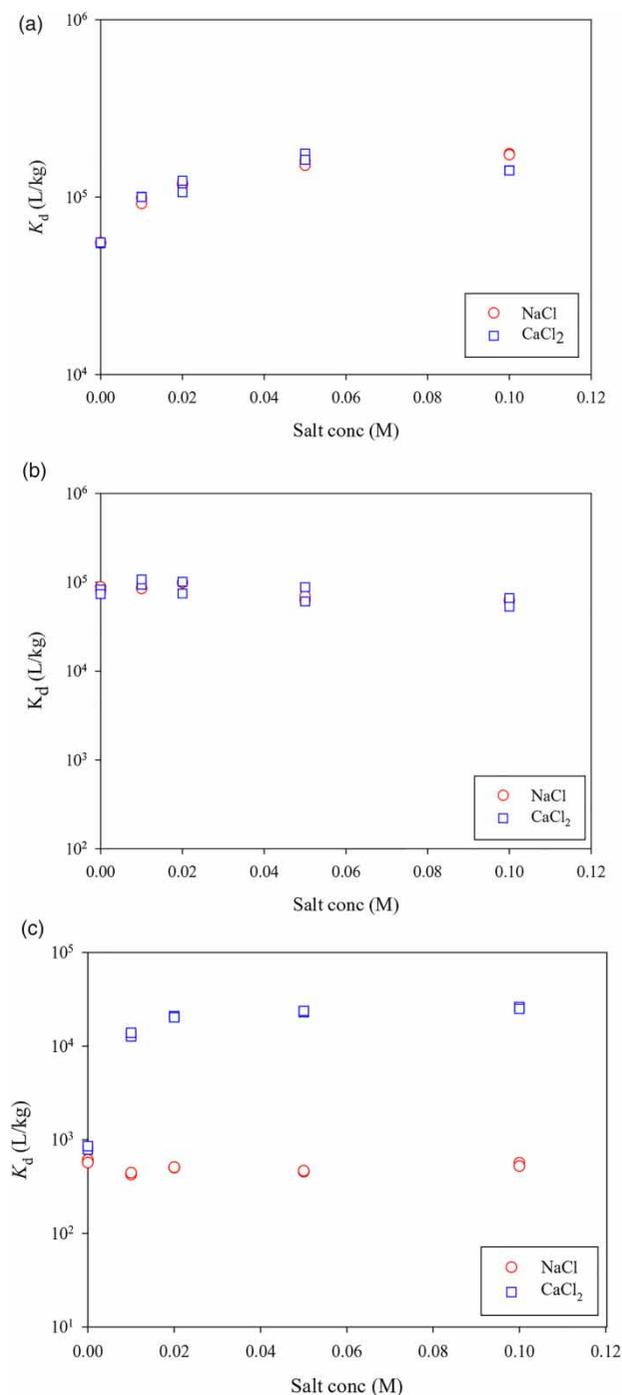
**Figure 4** | Pore size distributions of adsorbents before and after adsorption of different adsorbates: methylene blue (MB), methyl orange (MO) and chrysophenine G (CG). (a) CTF-1. (b) CTF<sub>DCBP</sub>.



**Figure 5** | Changes of adsorbent-to-solution distribution coefficients ( $K_d$ ) with pH at single point concentrations for adsorption of methylene blue (MB), methyl orange (MO) and chrysophenine G (CG) on CTF-1.

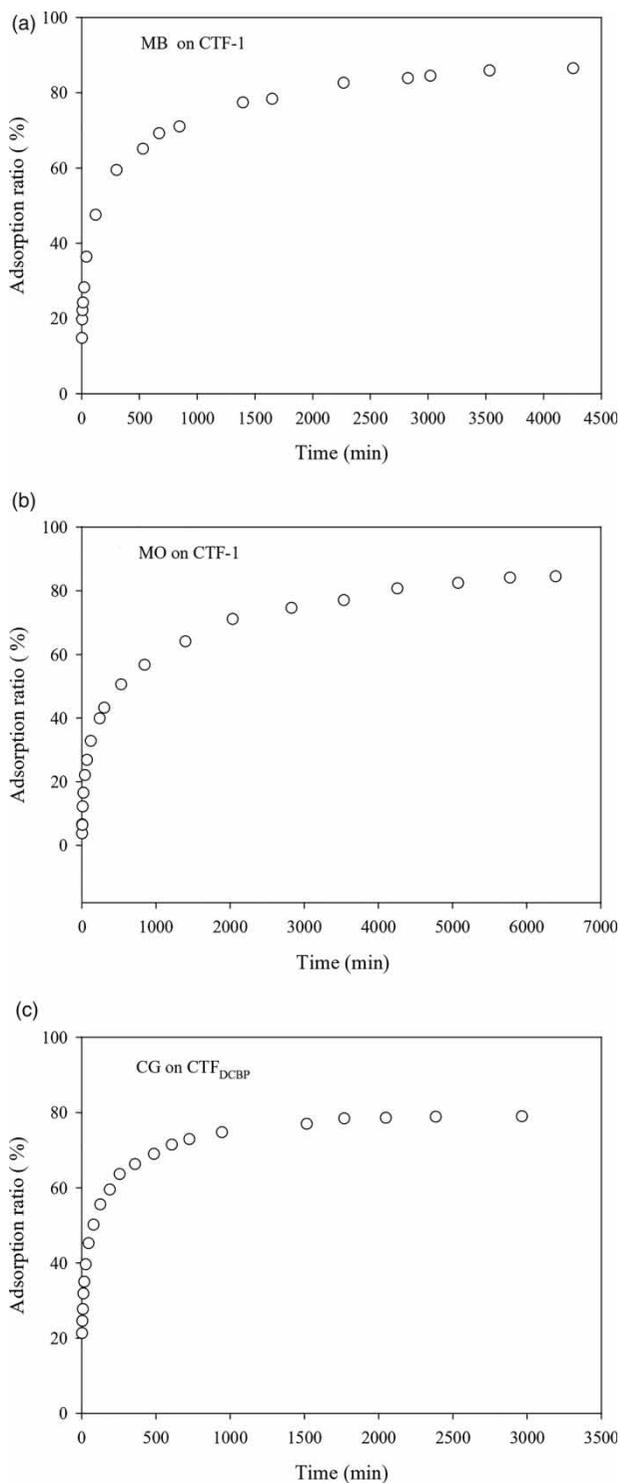
## Effects of pH and ionic strength

The effects of pH for three dyes on CTF-1 (CTF<sub>DCBP</sub> were not studied due to the similar pzc to CTF-1, only difference in pore structure) are presented in Figure 5. As



**Figure 6** | Effect of ionic strength (NaCl, CaCl<sub>2</sub>) on adsorption coefficient ( $K_d$ ) for single-point adsorption of dyes on CTF-1. (a) Methylene blue (MB). (b) Methyl orange (MO). (c) Chrysophenine G (CG).

shown in Figure 5, the  $K_d$  value increased gradually with the increasing pH for MB. MO and CG decrease with the increasing pH, suggesting the same adsorptive



**Figure 7** | Adsorption kinetics of dyes on CTFs. Methylene blue on CTF-1 (a), Methyl orange (MO) on CTF-1 (b), and Chrysophenine G (CG) on CTF<sub>DCBP</sub> (c).

**Table 2** | Fitting parameters for adsorption kinetics by pseudo-first-order and pseudo-second-order models

Dye/adsorbent	$q_{exp}/\text{mmol}\cdot\text{kg}^{-1}$	Pseudo-first-order kinetic model			Pseudo-second-order kinetic model		
		$k_1/1\cdot\text{s}^{-1}$	$q_{cal}/\text{mmol}\cdot\text{kg}^{-1}$	$R^2$	$k_2/\text{kg}\cdot(\text{mmol}^{-1}\cdot\text{s}^{-1})$	$q_{cal}/\text{mmol}\cdot\text{kg}^{-1}$	$R^2$
MB/CTF-1	577.90	$2.21 \times 10^{-4}$	353.29	0.972	$1.88 \times 10^{-6}$	581.39	0.997
MO/CTF-1	644.75	$1.41 \times 10^{-4}$	497.40	0.959	$7.31 \times 10^{-6}$	648.93	0.997
CG/CTF <sub>DCBP</sub>	938.14	$4.54 \times 10^{-4}$	468.82	0.972	$8.40 \times 10^{-5}$	946.07	0.999

interaction with CTF-1. CTF-1 is deprotonated and negatively charged with the increasing pH as the pzc around pH 7.2 (see SI Figure S6). Electrostatic interaction between cationic dye MB and CTF-1 gradually strengthened. However, the adsorption affinity could be suppressed when the pH continue increasing, because electrostatic repulsion was enhanced between CTF-1 and negatively charged MO and CG. In addition, adsorption decreased slightly at pH range 7.2–10, indicating that higher pH favored hydrogen bonding interaction with the deprotonated triazine structure.

The effects of ionic strength for dyes on CTF-1 are listed in Figure 6. Clearly, ionic strength promoted MB adsorption on CTF-1. Salting-out effect is responsible for the increasing adsorption coefficient for MB (Grover & Ryall 2005). Similar result has been report in previous studies (Fontecha-Cámara *et al.* 2007; Eren & Afsin 2008). The adsorption of MO and CG decreased with the increasing ionic strength. MO and CG as anionic dyes, the electrostatic screening of the surface charge gradually enhanced with the increasing counterion species, leading to the lower adsorption coefficient. However,  $\text{Ca}^{2+}$  promoted the adsorption of CG on CTF-1, which may be caused by coordination or complexation between  $\text{Ca}^{2+}$  and CG.

## Adsorption kinetics

Adsorption kinetics of MB and MO on CTF-1 and adsorption kinetics of CG on CTF<sub>DCBP</sub> are presented in Figure 7. As show in Figure 7, small molecular dyes MB and MO adsorption on CTF-1 reached equilibrium within 3,500 and 5,000 min separately. Of note, adsorption equilibrium for CG on CTF<sub>DCBP</sub> achieved equilibrium within 200 min. CTF-1 has narrow pore size distribution, and the dye molecules are not easy to diffuse into the interior, leading to relatively slow kinetics. The rapid kinetics for CTF<sub>DCBP</sub> correlated closely with the shaped, open and wide pore size distribution, which is consistent with the results of adsorbent pore size distribution.

In order to explain the mass transfer process during the dyes' adsorption, pseudo-first-order and pseudo-second-

order kinetic models were applied. As the following equation:

$$\log(q_e - q_t) = \log(q_e) - \frac{k_1 t}{2.303} \quad (3)$$

$$\frac{t}{q_t} = \frac{1}{k_2 q_e^2} - \frac{t}{q_e} \quad (4)$$

where  $q_e$  is the equilibrium adsorbed concentration,  $q_t$  is the adsorbed concentration at time  $t$ ,  $k_1$  and  $k_2$  are the pseudo-first order rate constant and the pseudo-second order rate constant, respectively.

Simulation results of dyes adsorption on CTFs based on the pseudo-first-order kinetics and pseudo-second-order kinetics are presented in SI Figure S7, and the fitting parameters are listed in Table 2. As shown in SI Figure S7(b), the plot of  $t/q_t$  versus  $t$  presented a linear relation with a higher  $R^2$  (0.997), suggesting that pseudo-second-order kinetic model could well depict the dyes' adsorption process to CTFs. In addition, the  $q_{exp}$  data (obtained from experimental data) are approximately identical to the  $q_{cal}$  data (calculated from the pseudo-second-order model) in Table 2, which further confirmed that the dyes' adsorption process on CTFs obeyed the pseudo-second-order kinetics model.

## CONCLUSIONS

In this study, two different covalent triazine-based frameworks were synthesized and their adsorption for three dyes was systematically investigated. Characterization results indicated that the CTFs were successfully synthesized with a homogeneous and regular-shaped structure. Adsorption results demonstrated that the selected three dyes have strong adsorption on CTFs adsorbents because of cation- $\pi$ , electrostatic interaction and hydrogen bonding interaction. Pore size distribution of CTFs is an important factor for adsorption particularly for bulky dyes CG. Acidic conditions are favorable for the adsorption of MB, while alkaline conditions are favorable for the adsorption of MO and CG. The

results in this study indicate that CTFs are promising adsorbents for adsorptive removal of dyes in aqueous solution

## ACKNOWLEDGEMENTS

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## DATA AVAILABILITY STATEMENT

All relevant data are included in the paper or its Supplementary Information.

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